

## Influence of nano-CeO<sub>2</sub> on coating structure and properties of electrodeposited Al/ $\alpha$ -PbO<sub>2</sub>/ $\beta$ -PbO<sub>2</sub>

Zhen CHEN<sup>1</sup>, Qiang YU<sup>1</sup>, Deng-hui LIAO<sup>2</sup>, Zhong-cheng GUO<sup>2</sup>, Jian WU<sup>2</sup>

1. Faculty of Science, Kunming University of Science and Technology, Kunming 650093, China;
2. Faculty of Metallurgy and Energy Engineering, Kunming University of Science and Technology, Kunming 650093, China

Received 6 April 2012; accepted 10 September 2012

**Abstract:** Al/ $\alpha$ -PbO<sub>2</sub>/ $\beta$ -PbO<sub>2</sub> composite electrodes doped with rare earth oxide (CeO<sub>2</sub>) were prepared by anodic oxidation method to investigate the influence of nano-CeO<sub>2</sub> dopants on the properties of Al/ $\alpha$ -PbO<sub>2</sub>/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> electrodes and the impact of  $\alpha$ -PbO<sub>2</sub> as the intermediate layer. The results show that using  $\alpha$ -PbO<sub>2</sub> as the intermediate layer will benefit the crystallization of  $\beta$ -PbO<sub>2</sub> and  $\beta$ -PbO<sub>2</sub> is more suitable as the surface layer than  $\alpha$ -PbO<sub>2</sub>. CeO<sub>2</sub> dopants change the crystallite size and crystal structure, enhance the catalytic activity, and even change the deposition mechanism of PbO<sub>2</sub>. The doping of CeO<sub>2</sub> in the PbO<sub>2</sub> electrodes can enhance the electro-catalytic activity, which is helpful for oxygen evolution, and therefore reduce the cell voltage.

**Key words:** rare earth; CeO<sub>2</sub>; composite electrode material;  $\alpha$ -PbO<sub>2</sub>;  $\beta$ -PbO<sub>2</sub>; cell voltage; inert anode

### 1 Introduction

Studies on inert anode materials used in zinc-plating industry have mostly focused on conventional anode materials, such as lead-based alloys, dimensionally stable anode, Au, Pt and glassy carbon [1–3]. However, the disadvantages of conventional anode materials including high cell voltage, poisonousness, low mechanical strength, inefficient conductivity and impurity product caused by anode re-dissolve have always perplexed us [4,5]. Therefore, further researches have been undertaken to discover more efficient electrode materials and metal oxide-film electrodes, such as PbO<sub>2</sub>, SnO<sub>2</sub> and RuO<sub>2</sub> [6–10].

Lead dioxide (PbO<sub>2</sub>) electrode has been extensively used in electrochemical industry and regarded as an excellent metal oxide electrode because of its low price compared with noble metals, good chemical stability, and high catalytic activity for oxygen evolution. The application of PbO<sub>2</sub> electrode is largely dependent upon its structure, morphology, and phase composition. In order to further improve the electrochemical properties of PbO<sub>2</sub> toward various applications, incorporating some

ions or particles such as rare earth into the film of lead oxide was investigated.

It is well known that PbO<sub>2</sub> has two different crystallographic forms: orthorhombic and tetragonal ( $\alpha$  and  $\beta$ ).  $\alpha$ -PbO<sub>2</sub> is obtained from alkaline solution and  $\beta$ -PbO<sub>2</sub> from acid solution [11].  $\alpha$ -PbO<sub>2</sub> has a better contact between particles, and a more compact structure than  $\beta$ -PbO<sub>2</sub>. Unfortunately, more compact structure leads to bad conductivity compared with  $\beta$ -PbO<sub>2</sub> [12]. Different electro-catalytic activities of  $\alpha$  and  $\beta$  forms of PbO<sub>2</sub> were observed in other studies. It was also observed that the structure of crystallization of PbO<sub>2</sub> films influenced the electro-catalytic properties of the material [13–19].

A new type of PbO<sub>2</sub> anode was widely used in electrolysis [20]. This electrode is made up of four layers: a metal base, a conductive layer (protecting the substrate from passivation),  $\alpha$ -PbO<sub>2</sub> as the intermediate layer, and  $\beta$ -PbO<sub>2</sub> as surface layer. Aluminum is relatively cheap and has a good conductivity. The electrode material by electrodepositing lead dioxide on Al substrate has huge market prospects. Rare earth oxides, as powerful oxidants, can easily catalyze the oxidation of organics. It was reported that [21–24] metal

oxides have been successfully doped into  $\text{PbO}_2$  electrodes by anodic codeposition. However, few researches on the doping of rare earth oxide into  $\text{PbO}_2$  electrodes have been reported.

In this work,  $\alpha\text{-PbO}_2$  was chosen as intermediate layer, and  $\beta\text{-PbO}_2$  as the surface layer.  $\text{Ce(IV)}$  was introduced as a doping agent into  $\text{PbO}_2$  electrode for its superior properties [25] were successfully doped by the anodic codeposition method. It changes the crystallite size and enhances the catalytic activity in the oxidation of the material. Scanning electron microscopy (SEM), X-ray diffraction (XRD) and energy-dispersive spectroscopy (EDS) were used to examine the changes in the coating.

## 2 Experimental

### 2.1 Preparation of coatings

After a series of pretreatments: sand blasting→degreasing (40 g/L  $\text{Na}_3\text{PO}_4$ , 10 g/L  $\text{Na}_4\text{SiO}_4$ , 3 min)→chemically etching (10 mL/L HF, 50 mL/L  $\text{HNO}_3$ , 90 s)→coating by a conductive layer, 1060# Al was used as an anode and machined to dimensions of 40 mm×10 mm×1 mm. Pure lead was used as a cathode. The electrodeposition of  $\alpha\text{-PbO}_2$  was conducted in an alkaline bath, while that of  $\beta\text{-PbO}_2$  was conducted in an aqueous bath. The plating conditions are listed in Table 1 and Table 2, respectively. Two types of anodes were made: one was Al/conductive layer/ $\beta\text{-PbO}_2$  (No. 1), and the other was Al/conductive layer/ $\alpha\text{-PbO}_2$ / $\beta\text{-PbO}_2$  (No. 2). The difference between them was the intermediate layer  $\alpha\text{-PbO}_2$ .  $\text{CeO}_2$  was introduced as a doping agent into the aqueous  $\beta\text{-PbO}_2$  electrolyte. By the anodic codeposition method,  $\text{CeO}_2$  was successfully doped into No. 2 electrode.

### 2.2 Measuring instruments

Micrographs of the coating surface were obtained by scanning electron microscopy (ESEM, FEI, Quanta200). The structures of the films were analyzed by X-ray diffraction (XRD) with  $\text{Co K}_\alpha$  radiation in a standard X-ray diffract meter (Rigaku D/max-1200X). The element contents were tested by energy-dispersive spectroscopy (EDAX-Phoenix). The over-potential was tested in 1.3 mol/L  $\text{ZnSO}_4$ +1 mol/L  $\text{H}_2\text{SO}_4$  (pH=4.5)

using polarization curves at a scanning rate of 50 mV/s. (CHI660D, Chenhua, China). During the measurement, a three-electrode system was used. The working electrode was the composite coating (1 cm×1 cm). The reference electrode was saturated calomel electrode (SCE) used directly in contact with the working solution. The counter electrode was platinum (1 cm×1 cm).The measurement was conducted at room temperature.

## 3 Results and discussion

### 3.1 Choice of intermediate layer

In this work,  $\alpha\text{-PbO}_2$  was obtained at a constant current density of 20 mA/cm<sup>2</sup> for 30 min in the solution containing 180 g/L NaOH saturated with PbO(s), and was used as the intermediate layer. A typical XRD pattern of  $\alpha\text{-PbO}_2$  deposited on Al/conductive layer is shown in Fig. 1. The surface morphology of  $\alpha\text{-PbO}_2$  coating is shown in Fig. 2. The XRD pattern indicates the presence of  $\alpha\text{-PbO}_2$ . The characteristic peaks are  $\alpha\text{-PbO}_2$  (scrutinyite), and  $\beta\text{-PbO}_2$  (plattnerite) is not observed. The grain of  $\alpha\text{-PbO}_2$  looks like rod or fiber. Numerous crystal edges and a few pores are found in such coating. However, these defects are proved to be helpful for the deposition of  $\beta\text{-PbO}_2$  in further study.

The XRD patterns of two types of  $\beta\text{-PbO}_2$  coatings (No. 1 and 2) shown in Fig. 3 all accord with the PDF#41—1492, which is plattnerite ( $\beta\text{-PbO}_2$ ). No. 1 was prepared directly on the Al conductive layer, while

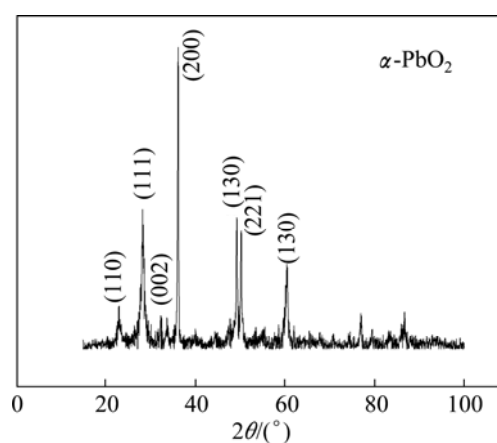


Fig. 1 XRD pattern of  $\alpha\text{-PbO}_2$  (scrutinyite)

Table 1 Deposition condition for  $\alpha\text{-PbO}_2$  coatings

$\rho(\text{NaOH})/(\text{g}\cdot\text{L}^{-1})$	PbO	Current density/ $(\text{mA}\cdot\text{cm}^{-2})$	pH	Temperature/ $^{\circ}\text{C}$	Plating time/min
180	Saturation	20	9.5–10	40–50	30–40

Table 2 Deposition condition for  $\beta\text{-PbO}_2$  coatings

$\rho(\text{Pb}(\text{NO}_3)_2)/(\text{g}\cdot\text{L}^{-1})$	$\rho(\text{Cu}(\text{NO}_3)_2)/(\text{g}\cdot\text{L}^{-1})$	$\rho(\text{NaF})/(\text{g}\cdot\text{L}^{-1})$	Current density/ $(\text{mA}\cdot\text{cm}^{-2})$	pH	Temperature/ $^{\circ}\text{C}$	Plating time/h
190	15	0.5	5	3–3.5	70–80	1

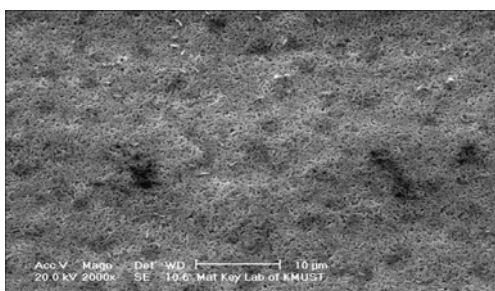


Fig. 2 SEM image of  $\alpha$ -PbO<sub>2</sub> coating (scrutinyite)

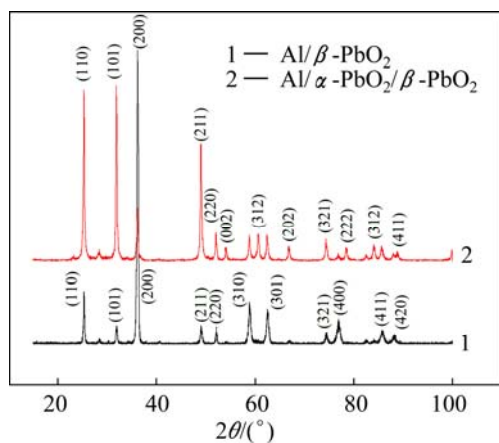


Fig. 3 XRD patterns of  $\beta$ -PbO<sub>2</sub> coatings

No. 2 was prepared on the  $\alpha$ -PbO<sub>2</sub> layer. The main crystal plane of No. 1 is (200), while that of No. 2 is (101). The main crystal plane of No. 2 is consistent with the results reported by ABACI et al [26]. Furthermore, No. 2 has more peaks: (002), (312), (202), (222), (312), and they are all consistent with the PDF#41–1492, showing that No. 2 is better crystallized. Apparently,  $\alpha$ -PbO<sub>2</sub> as intermediate layer will improve the crystallization of  $\beta$ -PbO<sub>2</sub>.

Table 3 shows the  $\Delta G_r^\ominus$  values of several substances, which may participate as a reactant or product in producing PbO<sub>2</sub>. Table 4 presents the  $\Delta G_r^\ominus$  of each reaction and demonstrates that thermodynamic reaction followed by ease of PbO>PbO<sub>2</sub>>Pb<sub>2</sub>O<sub>3</sub>>Pb<sub>3</sub>O<sub>4</sub>. Figure 4 shows that the precipitation potential of  $\alpha$ -PbO<sub>2</sub> is lower than that of  $\beta$ -PbO<sub>2</sub>, which requires small electromotive force ( $E$ ). So, according to the equation:  $\Delta G = -nEF$  ( $\Delta G > 0$ ), when the product is  $\alpha$ -PbO<sub>2</sub>, the  $\Delta G$  is low, the energy barrier is smaller and therefore the thermodynamic stability is poor. Researchers also conducted a study on this issue and came to conclusions that the thermodynamic stability of  $\beta$ -PbO<sub>2</sub> is better than that of  $\alpha$ -PbO<sub>2</sub> [29]. Above all, the thermodynamic reaction (precipitation potential) followed by ease of PbO> $\alpha$ -PbO<sub>2</sub>> $\beta$ -PbO<sub>2</sub>>Pb<sub>2</sub>O<sub>3</sub>>Pb<sub>3</sub>O<sub>4</sub>. In this case,  $\beta$ -PbO<sub>2</sub> coating is more suitable as a surface anode materials.

Table 3 Reactant and product of anodic process and  $\Delta G_r^\ominus$  [27,28]

Substance	$\Delta G_r^\ominus / (\text{kJ} \cdot \text{mol}^{-1})$
H <sub>2</sub> O	-306.39
H <sup>+</sup>	6.23
Pb <sup>2+</sup>	8.11
PbO	-238.43
Pb <sub>2</sub> O <sub>3</sub>	-531.01
Pb <sub>3</sub> O <sub>4</sub>	-781.13
PbO <sub>2</sub>	-295.59

Table 4 Reaction of anodic process and  $\Delta G_r^\ominus$  [27,28]

Reaction	$\Delta G_r^\ominus / (\text{kJ} \cdot \text{mol}^{-1})$
Pb <sup>2+</sup> +H <sub>2</sub> O→PbO+2H <sup>+</sup>	72.31
2Pb <sup>2+</sup> +3H <sub>2</sub> O→Pb <sub>2</sub> O <sub>3</sub> +6H <sup>+</sup> +2e	357.98
3Pb <sup>2+</sup> +4H <sub>2</sub> O→Pb <sub>3</sub> O <sub>4</sub> +8H <sup>+</sup> +2e	418.63
Pb <sup>2+</sup> +2H <sub>2</sub> O→PbO <sub>2</sub> +4H <sup>+</sup> +2e	282.65

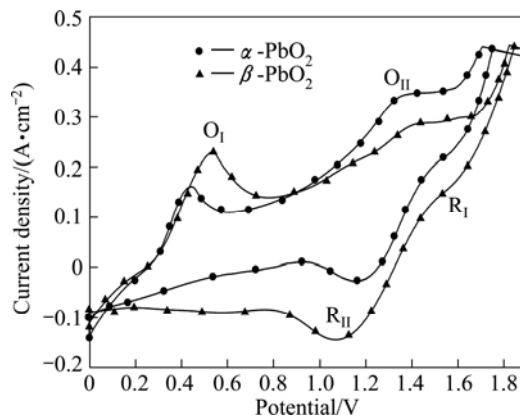


Fig. 4 CV curves of  $\alpha$ -PbO<sub>2</sub> and  $\beta$ -PbO<sub>2</sub> coatings (O<sub>I</sub>—Oxidation peak I; O<sub>II</sub>—Oxidation peak II; R<sub>I</sub>—Reduction I; R<sub>II</sub>—Reduction II)

Figure 5(a) presents the  $\beta$ -PbO<sub>2</sub> prepared directly on the conductive layer ( $\beta_D$ ), while Fig. 5(b) presents  $\beta$ -PbO<sub>2</sub> prepared on  $\alpha$ -PbO<sub>2</sub> layer ( $\alpha\beta$ ). The morphology of the  $\beta_D$  shown in Fig. 5(a) looks like a nappe sheet, whereas that of  $\alpha\beta$  looks like a typical pyramid and the average grain size is 25  $\mu\text{m}$ . It is obvious that coatings prepared on the  $\alpha$  layer are more compact and uniform. Studies show that [30–32],  $\alpha$ -PbO<sub>2</sub> intermediate layer can effectively increase the firmness of the lead dioxide coating and the substrate, and the ease of the distortion of electrodeposition, and make the surface layer  $\beta$ -PbO<sub>2</sub> distribute more uniformly. Therefore, new type of PbO<sub>2</sub> electrode is composed of  $\alpha$ -PbO<sub>2</sub> intermediate layer and  $\beta$ -PbO<sub>2</sub> surface layer, so a better catalytic activity is obtained [33].

### 3.2 CeO<sub>2</sub> as doping agent

The compositional analysis of Al/ $\alpha$ -PbO<sub>2</sub>/ $\beta$ -PbO<sub>2</sub> electrodeposits was performed under different CeO<sub>2</sub>

concentrations in bath using energy dispersive spectroscopy. EDS spectra of  $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> films deposited under different conditions are shown in Fig. 6.

It is found from Fig. 6 that with increasing the CeO<sub>2</sub> concentration in bath from 10 to 50 g/L, Ce contents are 2.97%, 2.90%, 3.47%, 3.44% and 3.73%, respectively.

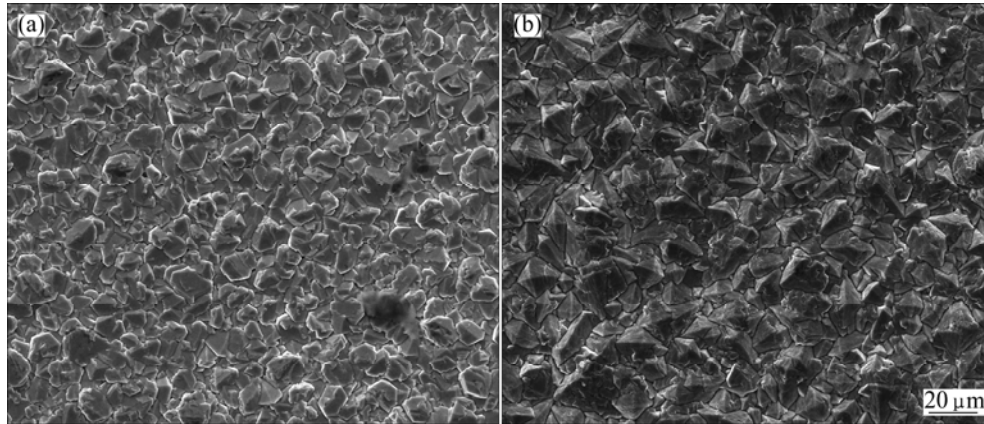


Fig. 5 SEM images of  $\beta$ -PbO<sub>2</sub> prepared directly on conductive layer (a) and on  $\alpha$ -PbO<sub>2</sub> layer (b)

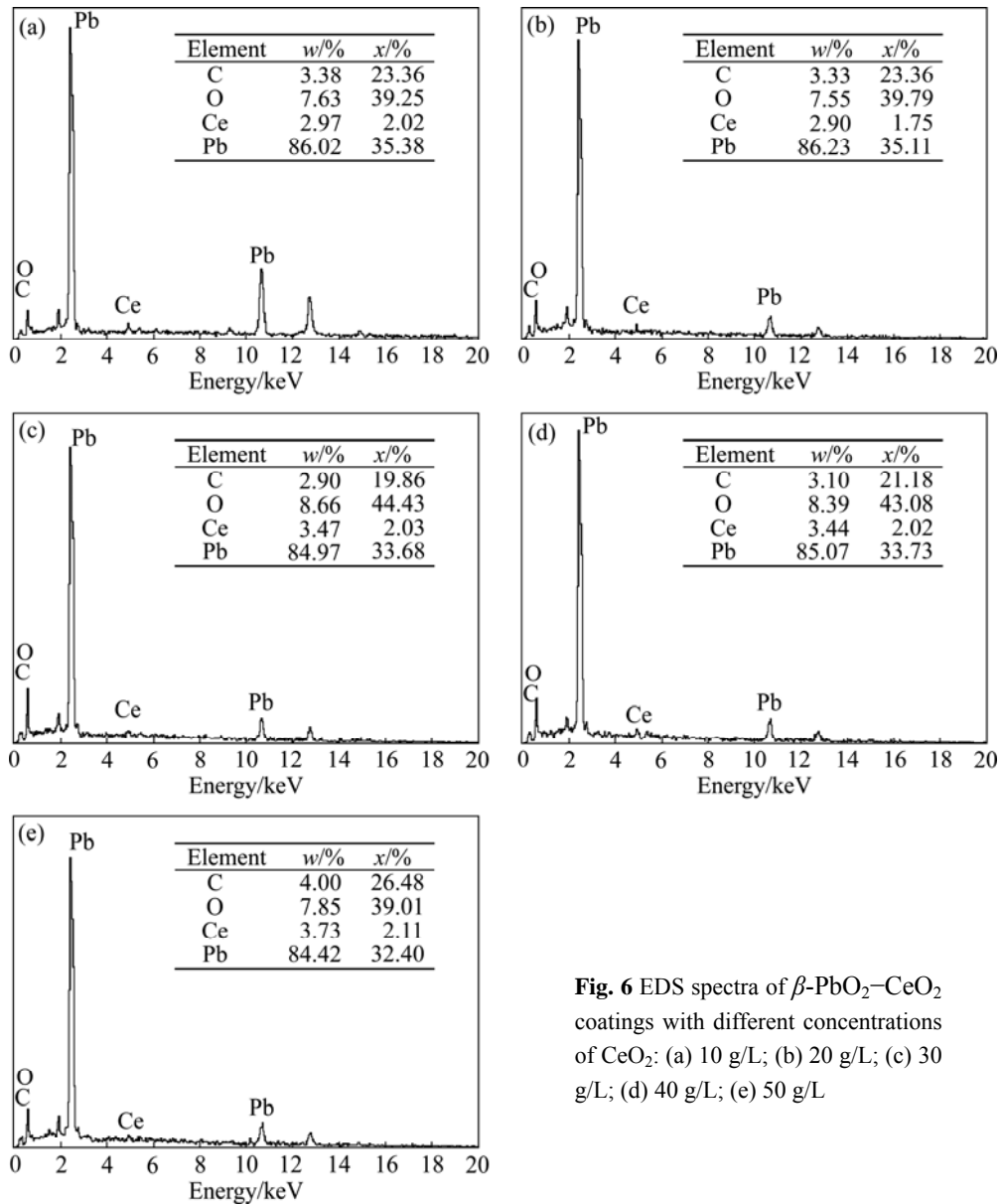
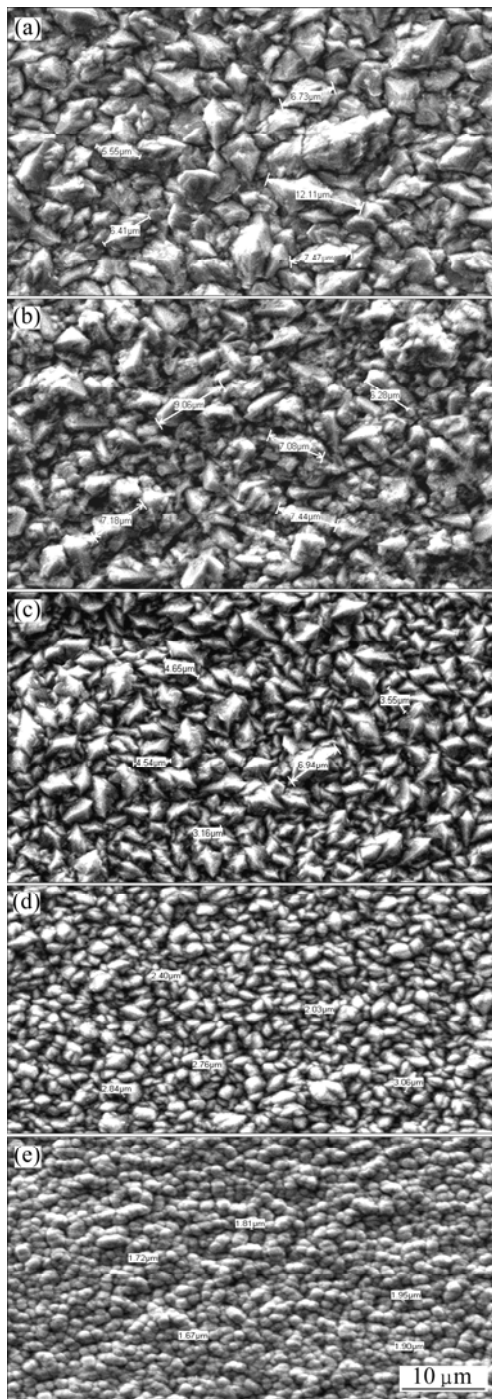


Fig. 6 EDS spectra of  $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> coatings with different concentrations of CeO<sub>2</sub>: (a) 10 g/L; (b) 20 g/L; (c) 30 g/L; (d) 40 g/L; (e) 50 g/L

Obviously, particles will get more opportunity to be embed into  $\text{Al}/\alpha\text{-PbO}_2/\beta\text{-PbO}_2$  composite by adding more nucleation points on the anodic surface. More particles suspending in the electrolyte are good for  $\text{CeO}_2$  to stay, absorb and form nucleation points. As a result, increasing the  $\text{CeO}_2$  concentration will surely help the co-deposition. Rare earth oxides can easily catalyze the oxidation of organics and change the surface morphology.

When ceria dioxide is used, as shown in Fig. 7, the



**Fig. 7** SEM images of  $\beta\text{-PbO}_2$  with different concentrations of  $\text{CeO}_2$ : (a) 10 g/L; (b) 20 g/L; (c) 30 g/L; (d) 40 g/L; (e) 50 g/L

surface morphology presents nodular shape. The average grain sizes decrease with the increase of Ce content. The average grain sizes are shown in Table 5. The present experimental results indicate that the crystallization process of  $\text{PbO}_2$  can be affected by adulteration of  $\text{CeO}_2$ , thus changing surface microstructure of the coating. The average grain size of  $\text{PbO}_2$  decreases with the adulteration of  $\text{CeO}_2$  because the doped ceria dioxide provides a new center for  $\text{PbO}_2$  to nucleate, which hinders the further growth of  $\text{PbO}_2$ . In other words, the nucleation rate is faster than the growing rate [34].

**Table 5** Grain size of coatings

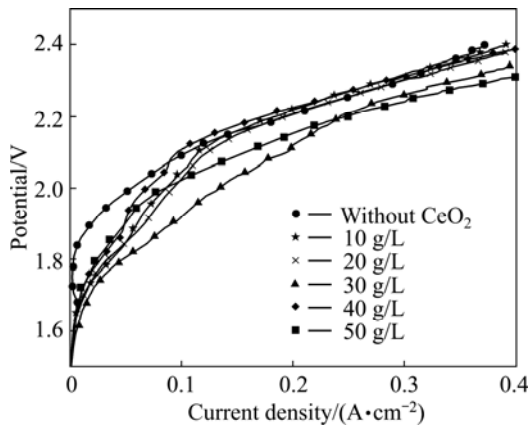
Sample No.	Minimum size/ $\mu\text{m}$	Maximum size/ $\mu\text{m}$	Average size/ $\mu\text{m}$
1	5.55	12.11	7.67
2	6.28	9.06	7.408
3	3.16	6.94	4.568
4	2.03	3.06	2.618
5	1.67	1.95	1.81

### 3.3 Over potential and catalytic activity for oxygen evolution

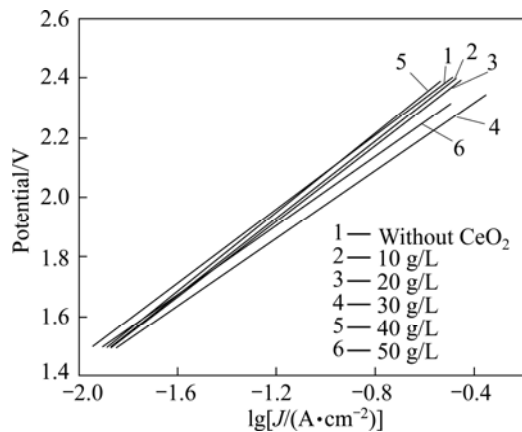
In zinc plating industry, anodic over potential, mainly caused by oxygen evolution reaction, will consume a large percentage of cell voltage. Therefore, a low oxygen evolution potential will save electricity and reduce the cell voltage a lot. Figure 8 gives the polarization curves of  $\text{Al}/\alpha\text{-PbO}_2/\beta\text{-PbO}_2\text{-CeO}_2$  and  $\text{Al}/\beta\text{-PbO}_2$  electrodes in 1.3 mol/L  $\text{ZnSO}_4$ +1 mol/L  $\text{H}_2\text{SO}_4$  (pH=4.5). Compared with  $\text{Al}/\alpha\text{-PbO}_2/\beta\text{-PbO}_2$ , adulteration of  $\text{CeO}_2$  can apparently lower the over-potential of  $\text{PbO}_2$ . According to the Tafel equation:

$$\eta = -\frac{2.3RT}{n\beta F} \lg J^0 + \frac{2.3RT}{n\beta F} \lg J$$

where  $\beta$  is the transfer coefficient and  $J^0$  is the exchange current density, dividing the intercept of linear by its slope,  $J^0$  can be obtained, and the fitting curves are shown in Fig. 9. The exchange current densities are listed in Table 6, confirming that  $\text{Al}/\alpha\text{-PbO}_2/\beta\text{-PbO}_2\text{-CeO}_2$  has a higher catalytic activity for oxygen evolution than  $\text{Al}/\beta\text{-PbO}_2$ . Moreover, adulteration of  $\text{CeO}_2$  can greatly influence the exchange current. When  $\text{CeO}_2$  concentration in bath is 30 g/L, the exchange current of  $\text{Al}/\alpha\text{-PbO}_2/\beta\text{-PbO}_2\text{-CeO}_2$  electrode is the highest, indicating that the content of Ce can easily catalyze the oxidation of organics. On the other hand, the surface structure of  $\text{PbO}_2$  has a strong influence on the catalytic activity for oxygen evolution [35–37]. The SEM images of  $\text{Al}/\alpha\text{-PbO}_2/\beta\text{-PbO}_2\text{-CeO}_2$  and  $\text{Al}/\alpha\text{-PbO}_2/\beta\text{-PbO}_2$  electrode show that the morphologies of the two types of electrodes are rather different. The surface of  $\text{Al}/\alpha\text{-PbO}_2/$



**Fig. 8** Polarization curves of PbO<sub>2</sub> electrodes prepared with different concentrations of CeO<sub>2</sub> in bath



**Fig. 9** Linear fitting of polarization curves of PbO<sub>2</sub> electrodes prepared with different concentrations of CeO<sub>2</sub> in bath

**Table 6** Kinetic parameters of oxygen evolution

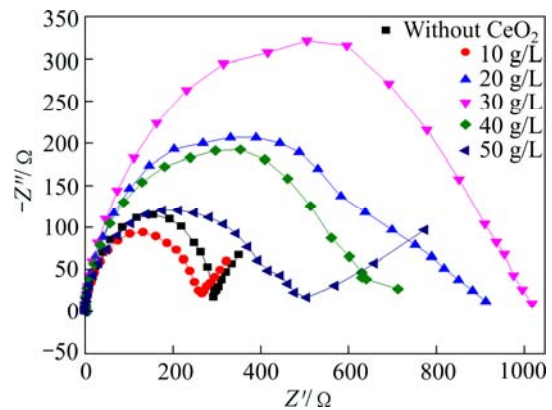
$\rho(\text{CeO}_2)/(\text{g}\cdot\text{L}^{-1})$	$a/\text{V}$	$b/(\text{V}\cdot\text{A}^{-1})$	$J^0/(\text{A}\cdot\text{cm}^{-2})$
0	2.535	0.393	$3.59\times 10^{-7}$
10	2.599	0.518	$9.73\times 10^{-6}$
20	2.562	0.515	$5.99\times 10^{-6}$
30	2.637	0.467	$1.07\times 10^{-5}$
40	2.522	0.486	$5.46\times 10^{-6}$
50	2.529	0.450	$5.89\times 10^{-6}$

$a$ : Slope;  $b$ : Intercept;  $J^0$ : Exchange current density.

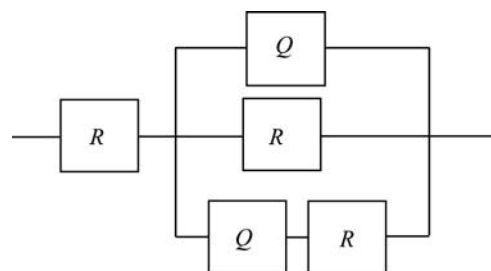
$\beta$ -PbO<sub>2</sub> electrode presents many micro-cracks, and looks like a typical pyramid shape; the grains are more dispersive and large. Al/ $\alpha$ -PbO<sub>2</sub>/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> is quite compact, and the grain size decreases. Therefore, the active surface area of Al/ $\alpha$ -PbO<sub>2</sub>/ $\beta$ -PbO<sub>2</sub>-CeO<sub>2</sub> electrode is larger than that of Al/ $\beta$ -PbO<sub>2</sub>. Moreover, electronic conduction exists in the rare earth oxides [38]. This demonstrates that ceria dioxide, as the catalytic sites, could strengthen the interface electron transfer of the electrode.

### 3.4 AC impedance

Figure 10 shows the Nyquist plots of the coatings prepared under different CeO<sub>2</sub> concentrations. It can be seen that when CeO<sub>2</sub> concentrations are 10 and 50 g/L, the plots are not the same as the others. Apparently, CeO<sub>2</sub> as a doping agent changes the reaction mechanism. Coatings, which were prepared under CeO<sub>2</sub> concentrations of 10 and 50 g/L, are coarse or can easily fall off. Therefore, only the other three were computed and analyzed. When CeO<sub>2</sub> concentration is 20–40 g/L, polarization resistance ( $R_p$ ) becomes large first and then gets small. When the fitting software (ZSimpWin) is used to fit and interpret the Nyquist plots, the obtained equivalent circuit is shown in Fig. 11 and the impedance fitting values are listed in Table 7. The equivalent circuit is composed of a solution resistance ( $R_s$ ), two constant phase elements  $Q$  (CPE) which represent the coating capacitance and the double layer capacitance, a coating resistance and a charge transfer resistance ( $R_{ct}$ ). Generally, CPE/Q may exist because of the rough surface or uneven distribution of the electric field [39]. Table 7 shows that the values of  $n_1$  are all equal to 1, indicating that dispersion effect does not occur between the solution/coating layers. While values of  $n_2$  are all not equal to 1, indicating that dispersion effect occurs under the coating layer, or maybe occurs in electric double layer. When the value of  $n_2$  is closer to 1, the coating layer is smoother and dispersion effect is weaker. When



**Fig. 10** Nyquist plots of coatings with different CeO<sub>2</sub> concentrations



**Fig. 11** Equivalent circuit of composite coatings in zinc plating solution

**Table 7** Fitting parameters of equivalent circuit of electrode

$\rho(\text{CeO}_2)/(\text{g}\cdot\text{L}^{-1})$	$R_s/(\Omega\cdot\text{m}^{-2})$	$Q_1(\text{CPE})/(\mu\text{F}\cdot\text{m}^{-2})$	$n_1$	$R_d/(\Omega\cdot\text{m}^{-2})$	$Q_2(\text{CPE})/(\mu\text{F}\cdot\text{m}^{-2})$	$n_2$	$R_{ct}/(\Omega\cdot\text{m}^{-2})$
20	0.6648	$1.183\times 10^{-5}$	1	840.1	$8.571\times 10^{-5}$	0.6447	605.4
30	0.6321	$8.409\times 10^{-6}$	1	998.9	$4.03\times 10^{-5}$	0.6957	686.1
40	0.6402	$1.363\times 10^{-5}$	1	302.4	$6.11\times 10^{-4}$	0.4641	447.5

CeO<sub>2</sub> concentration is 30 g/L, dispersion effect of the coating is weaker in that  $n_2$  is maximum, which demonstrates a smoother surface. It is considered that in the low-frequency area, the corrosion resistance of the composite coatings can be reflected by the impedance. Such impedance corresponds to the the charge transfer resistance ( $R_{ct}$ ).  $R_{ct}$  of the three coatings is not very different, only about 100  $\Omega/\text{cm}^2$ . As the same as the dispersion effect, the largest  $R_{ct}$  is tested on the coating when CeO<sub>2</sub> concentration is 30 g/L. This is probably because CeO<sub>2</sub> particles are firstly absorbed on the coating surface, by lowing the reaction area, formation of the oxidation and hydrated layer was hindered, and therefore  $R_{ct}$  increases. When CeO<sub>2</sub> particles are wrapped into the metal composite, the reaction area or active area is exposed again, oxidation and hydration occur, and then  $R_{ct}$  decreases. This is probable why coatings will have different mechanisms when prepared with different CeO<sub>2</sub> concentrations. Particles experience a complex process, including adsorption→desorption→inlay→coating. So the composite deposition process is actually complicated.

#### 4 Conclusions

1)  $\alpha$ -PbO<sub>2</sub> as intermediate layer can improve the deposition of  $\beta$ -PbO<sub>2</sub>, including structure and crystal plane.  $\beta$ -PbO<sub>2</sub> has better thermodynamic stability, and is more suitable as a surface layer.

2) Rare earth oxide dopants can decrease the grain size of PbO<sub>2</sub> and enlarge the active surface area and therefore change the content of Ce element in the coating.

3) The change of catalytic activity is mainly due to the specific role of the doped ceria dioxide and the different structures of electrodes.

#### References

- [1] ZHI G Y, HUI M M, DONG B S. New degradation mechanism of Ti/IrO<sub>2</sub>+MnO<sub>2</sub> anode for oxygen evolution in 0.5 M H<sub>2</sub>SO<sub>4</sub> solution [J]. *Electrochimica Acta*, 2008, 53(18): 5639–5643.
- [2] PANICA V V, JOVANOVICA V M, TERZICA S I, BARSOUMB M W, JOVIC V D, DEKANSKIA A B. The properties of electroactive ruthenium oxide coatings supported by titanium-based ternary carbides [J]. *Surface and Coatings Technology*, 2007, 202: 319–324.
- [3] AROMAA J, FORSEN O. Evaluation of the electrochemical activity of a Ti–RuO<sub>2</sub>–TiO<sub>2</sub> permanent anode [J]. *Electrochimica Acta*, 2006, 51(27): 6104–6110.
- [4] ZHAO Q, LIU Y, MULLER-STEINHAGEN H, LIU G. Graded Ni–P–PTFE coatings and their potential applications [J]. *Surface and Coatings Technology*, 2002, 155: 279–284.
- [5] FENG Q Y, LI T J, JIN J Z. Research on the mechanism of composite electroplating and its latest progress rare metal materials and engineering [J]. *Rare Metal Materials and Engineering*, 2007, 36(3): 559–564. (in Chinese)
- [6] BIRAME B, ENRIC B, BEATRICE M, PIERRE ALAIN M, CHRISTOS C, GIUSEPPE F, GIANCARL S. Electrochemical incineration of chloromethylphenoxy herbicides in acid medium by anodic oxidation with boron-doped diamond electrode [J]. *Electrochim Acta*, 2006, 51(15): 2872–2880.
- [7] CARLOS A M H, MARCO A Q, CHRISTOS C, SERGIO F, ACHILLE D B. Electrochemical incineration of chloranilic acid using Ti/IrO<sub>2</sub>, Pb/PbO<sub>2</sub> and Si/BDD electrodes [J]. *Electrochim Acta*, 2004, 50(4): 949–956.
- [8] CARMEM L P S Z, PIERRE-ALAN M, CHRISTOS C, ADALGISA R, DE A, JULIEN F C B. Electrochemical oxidation of p-chlorophenol on SnO<sub>2</sub>–Sb<sub>2</sub>O<sub>5</sub> based anodes for wastewater treatment [J]. *Journal of Applied Electrochemistry*, 2003, 33(12): 1211–1215.
- [9] PANIC V V, DEKANSKI A B, VIDAKOVIC T R, MISKOVIC-STANKOVIC V B, JAVANOVIC B Z, NIKOLIC V Z. Oxidation of phenol on RuO<sub>2</sub>–TiO<sub>2</sub>/Ti anodes [J]. *Solid State Electrochem*, 2005, 9(1): 43–54.
- [10] WANG Y H, CHENG S, CHAN K Y, LI X Y. Electrolytic generation of ozone on antimony- and nickel-doped tin oxide electrode [J]. *Journal of The Electrochemical Society*, 2005, 152(11): D197–D200.
- [11] CARR J P, HAMPSON N A. The lead dioxide electrode [J]. *Chemical Reviews*, 1972, 72(6): 679–702.
- [12] PETERSSON I, AHLBERG E, BERGHULT B. Parameters influencing the ratio between electrochemically formed  $\alpha$  and  $\beta$ -PbO<sub>2</sub> [J]. *Journal of Power Sources*, 1998, 76(1): 98–105.
- [13] AMADELLI R, MALDOTTI A, MOLINARI A, DANILOV F I, VELICHENKO A B. Influence of the electrode history and effects of the electrolyte composition and temperature on O<sub>2</sub> evolution at  $\beta$ -PbO<sub>2</sub> anodes in acid media [J]. *Journal of Electroanalytical Chemistry*, 2002, 534(1): 1–12.
- [14] PAVLOV D, MONAHOV B. Mechanism of the elementary electrochemical processes taking place during oxygen evolution on the lead dioxide electrode [J]. *Journal of The Electrochemical Society*, 1996, 143(11): 3616–3629.
- [15] MUNICHANDRAIA N, SATHYANARAYANA S. Insoluble anode of  $\alpha$ -lead dioxide coated on titanium for electrosynthesis of sodium perchlorate [J]. *Journal of Applied Electrochemistry*, 1988, 18(2): 314–316.
- [16] ABACI S, PEKMEZ K, PEKMEZ P, YILDIZ A. Electrocatalysis of polyaniline formation by PbO<sub>2</sub> in acetonitrile [J]. *Journal of Applied Polymer Science*, 2003, 87(4): 599–605.
- [17] ABACI S, TAMER U, PEKMEZ K, YILDIZ A. Electrosynthesis of 4,4'-dinitroazobenzene on PbO<sub>2</sub> electrodes [J]. *Journal of Applied*

- Electrochemistry, 2002, 32(2): 193–196.
- [18] ABACI S, YILDIZ A. Electropolymerization of thiophene and 3-methylthiophene on PbO<sub>2</sub> electrodes [J]. Journal of Electroanalytical Chemistry, 2004, 569(1): 161–168.
- [19] VELICHENKO A B, AMADELLI R, BENEDETTI A, GIRENKO D V, KOVALYOV S V, DANILOVA F I. Electrosynthesis and physicochemical properties of PbO<sub>2</sub> films [J]. Journal of The Electrochemical Society, 2002, 149(9): C445–C449.
- [20] UEDA M, WATANABE A, KAMEYAMA T, MATSUMOTO Y, SEKIMOTO M, SHIMAMUNE T. Performance characteristics of a new type of lead dioxide-coated titanium anode [J]. Journal of Applied Electrochemistry, 1995, 25: 817–822.
- [21] CATTARIN S, GUERRIERO P, MUSIANI M. Preparation of anodes for oxygen evolution by electrodeposition of composite Pb and Co oxides [J]. Electrochim Acta, 2001, 46(26–27): 4229–4234.
- [22] CATTARIN S, FRATEUR I, GUERRIERO P, MUSIANI M. Electrodeposition of PbO<sub>2</sub>+CoO<sub>x</sub> composites by simultaneous oxidation of Pb<sup>2+</sup> and Co<sup>2+</sup> and their use as anodes for O<sub>2</sub> evolution [J]. Electrochim Acta, 2000, 45: 2279–2288.
- [23] MUSIANI M, GUERRIERO P. Oxygen evolution reaction at composite anodes containing Co<sub>3</sub>O<sub>4</sub> particles [J]. Electrochim Acta, 1998, 44(8–9): 1499–1507.
- [24] MUSIANI M, FURLANETTO F, GUERRIERO P. Electrochemical deposition and properties of PbO<sub>2</sub>+Co<sub>3</sub>O<sub>4</sub> composites [J]. Journal of Electroanalytical Chemistry, 1997, 440(1–2): 131–138.
- [25] SRIVASTAVA M, WILLIAM GRIPS V K, RAJAM K S. Electrodeposition of Ni–Co composites containing nano-CeO<sub>2</sub> and their structure, properties [J]. Applied Surface Science, 2010, 257(3): 717–722.
- [26] ABACI S, PEKMEZ K, HOKELEK T, YILDIZ A. Investigation of some parameters influencing electrocrystallisation of PbO<sub>2</sub> [J]. Journal of Power Sources, 2000, 88(2): 232–236.
- [27] LI Di. Electrochemical principle [M]. Beijing: Beihang University Press, 1999. (in Chinese)
- [28] LI Wen-chao. Metallurgical and materials physical chemistry [M]. Beijing: Metallurgical Industry Press, 2001. (in Chinese)
- [29] ZHOU Ya-ning, WAN Ya-zhen, LIU Jin-dun. Preparation and application of PbO<sub>2</sub> electrode [J]. Salt Industry, 2006, 38(10): 8–11. (in Chinese)
- [30] WENG Feng, YU Bin. Preliminary research of determining COD using Pt/PbO<sub>2</sub> electrode [J]. Journal of Nanjing University of Technology, 2002, 24(2): 93–96.
- [31] PETERSSON I, AHLBERG E, BERGHULT B. Parameters influencing the ratio between electro-chemically formed  $\alpha$  and  $\beta$ -PbO<sub>2</sub> [J]. Journal of Power Sources, 1988, 76(1): 98–105.
- [32] FUKASAWA A. Production of commercial large lead dioxide electrode-application of a new-type lead dioxide electrode to electrolytic refining [J]. Mining and Metallurgical Institute of Japan, 1984, 1157: 599–602.
- [33] ZHANG Zhao-xian. Titanium electrode industry [M]. Beijing: Metallurgical Industry Press, 2000. (in Chinese)
- [34] CASELLATO U, CATTARIN S, MUSIANI M. Preparation of porous PbO<sub>2</sub> electrodes by electrochemical deposition of composites [J]. Electrochim Acta, 2003, 48(27): 3991–3998.
- [35] AMADELLI R, ARMELAO L, VELICHENKO A B, NIKOLENKO N V, GIRENKO D V, KOVALYOV S V, DANILOV F I. Oxygen and ozone evolution at fluoride modified lead dioxide electrodes [J]. Electrochim Acta, 1999, 45: 713–720.
- [36] ABACI S, PEKMEZ K, HOKELEK, YILDIZ A. Investigation of some parameters influencing electrocrystallisation of PbO<sub>2</sub> [J]. Journal of Power Sources, 2000, 88(2): 232–236.
- [37] HO J C K, TREMILIOSI G, SIMPRAGA R, CONWAY B E. Structure influence on electrocatalysis and adsorption of intermediates in the anodic O<sub>2</sub> evolution at dimorphic  $\alpha$ -PbO<sub>2</sub> and  $\beta$ -PbO<sub>2</sub> [J]. Journal of Electroanalytical Chemistry, 1994, 366(5):147–162.
- [38] MINACHEV F M. The application of rare earth for catalyst [M]. Beijing: Science Press, 1987. (in Chinese)
- [39] LU Chang-feng, LU Min-xu, ZHAO Guo-xian, BAI Zhen-quan, YAN Mi-lin, YANG Yan-qing. The analysis of electrode reactions of CO<sub>2</sub> corrosion of N80 steel [J]. Acta Metallurgica Sinica, 2002, 38(7): 770–774. (in Chinese)

## 纳米 CeO<sub>2</sub> 对电沉积 Al/ $\alpha$ -PbO<sub>2</sub>/ $\beta$ -PbO<sub>2</sub> 镀层结构和性能的影响

陈 阵<sup>1</sup>, 余 强<sup>1</sup>, 廖登辉<sup>2</sup>, 郭忠诚<sup>2</sup>, 武 剑<sup>2</sup>

1. 昆明理工大学 理学院, 昆明 650093;

2. 昆明理工大学 冶金与能源工程学院, 昆明 650093

**摘 要:** 采用阳极氧化法制备掺杂稀土氧化物(CeO<sub>2</sub>)的 Al/ $\alpha$ -PbO<sub>2</sub>/ $\beta$ -PbO<sub>2</sub> 复合电极, 考察 CeO<sub>2</sub> 的掺杂以及  $\alpha$ -PbO<sub>2</sub> 作为中间层对 Al/ $\alpha$ -PbO<sub>2</sub>/ $\beta$ -PbO<sub>2</sub> 电极性能的影响。结果表明:  $\alpha$ -PbO<sub>2</sub> 作为中间层有利于  $\beta$ -PbO<sub>2</sub> 的结晶,  $\beta$ -PbO<sub>2</sub> 比  $\alpha$ -PbO<sub>2</sub> 更适合作电极表层; CeO<sub>2</sub> 的掺杂能够改变晶粒尺寸和晶粒结构, 提高电极的催化活性, 并改变 PbO<sub>2</sub> 晶粒的沉积机理; 掺杂 CeO<sub>2</sub> 的 PbO<sub>2</sub> 电极的电催化活性能得到有效提高, 从而降低析氧电位和槽电压。

**关键词:** 稀土; CeO<sub>2</sub>; 复合电极材料;  $\alpha$ -PbO<sub>2</sub>;  $\beta$ -PbO<sub>2</sub>; 槽电压; 惰性阳极

(Edited by Xiang-qun LI)