

Available online at www.sciencedirect.com



Transactions of Nonferrous Metals Society of China

www.tnmsc.cn



Trans. Nonferrous Met. Soc. China 32(2022) 1705-1717

Microscopic mechanism of perfluorocarbon gas formation in aluminum electrolysis process

Ke-na SUN^{1,2}, Jie LI^{1,2}, Hong-liang ZHANG^{1,2}, Tian-shuang LI^{1,2}

 School of Metallurgy and Environment, Central South University, Changsha 410083, China;
National Engineering Research Center for Low-carbon Nonferrous Metallurgy, Central South University, Changsha 410083, China

Received 13 November 2021; accepted 7 March 2022

Abstract: In view of the unclear cause of perfluorocarbons (PFCs) emission in the anode effect stage of aluminum electrolysis, the microscopic formation mechanism of PFCs was studied by density functional theory calculation and X-ray photoelectron spectroscopy (XPS). It is found that the discharge of fluorine containing anions ($[F]^-$) on carbon anode first causes the substitution of C—H by C—F and further results in the saturation of aromatic C—C bonds, leading to the appearance of —CF₃ or —C₂F₅ group through six-carbon-ring opening. Elimination of —CF₃ and —C₂F₅ with F atom could be a likely mechanism of CF₄ and C₂F₆ formation. XPS results confirm that different types of —CF_x group can be formed on anode surface during electrolysis, and the possibility that $[F]^-$ discharges continuously at the C edge and finally forms different C—F bonds in quantum mechanical calculation was verified.

Key words: microscopic formation mechanism; aluminum electrolysis; perfluorocarbon gas; density functional theory calculation

1 Introduction

Perfluorocarbons (PFCs), typically CF₄ and C_2F_6 [1], are substances that are closely related to global warming due to their high equivalent greenhouse effect, which is 6500–9200 times that of CO₂ [2,3]. Recent studies have confirmed that the aluminum electrolysis industry is the world's largest emission source of PFCs, accounting for about 90% of the total emission of PFCs [4,5]. Considering the huge primary aluminum output of China (57% of the world's total) and the developing trend of carbon emission reduction, controlling the emission of PFCs from aluminum electrolysis is very imperative [6].

Aluminum electrolysis is a complex electrochemical process involving multiple reactants and products. The electrolyte used in aluminum electrolysis contains a variety of aluminum-fluoride and aluminum-oxy-fluoride anions [7,8], and each anion may discharge on the surface of carbon anode. In a normal electrolysis process, aluminum oxyfluoride coordination ions $([O]^{2-})$ in molten salt discharge and react with carbon to produce CO₂ and CO [9,10]. However, because of the up-sizing of aluminum electrolytic cells (500-600 kA) for practical production, alumina concentration in the cell is inhomogeneous, which leads to frequent local anode effect [11,12]. It is widely accepted that the bubbles at the bottom of the anode would aggregate and thus hinder electric current passing through electrolysis to the anode when alumina concentration is consumed to the critical value, leading to the increase of cell voltage and further [F]⁻ (aluminum-fluorine coordination ions in molten salt) discharge at the electrolyte/anode interface. As a consequence, PFC is formed and

DOI: 10.1016/S1003-6326(22)65904-1

Corresponding author: Hong-liang ZHANG, Tel: +86-13574831278, E-mail:csu13574831278@csu.edu.cn; Tian-shuang LI, Tel: +86-18613977386, E-mail:llmxq1234@csu.edu.cn

^{1003-6326/© 2022} The Nonferrous Metals Society of China. Published by Elsevier Ltd & Science Press

subsequently emitted in anode exhaust [13,14]. The anode gas generated during anode effect is composed of 2%-10% CO₂, 70%-80% CO, 10%-20% CF₄ and 1%-3% C₂F₆ [15,16].

Though aluminum electrolysis technology is mature and has been applied for decades, the PFC formation mechanism during anode effect remains ambiguous. LEBER et al [17] and MARKS et al [18-20] found that the increase of voltage in anode effect would lead to PFC generation. TABEREAUX [21], and NISSEN and SADOWAY [22] commented that C_2F_6 formation only occurs in the early stage of anode effect. The generation rate and duration of C₂F₆ are much lower than CF₄. QIN et al [23,24] declared that PFC emission increases with the increase of cell voltage during anode effect; however, it can still remain for an additional period after anode effect. ZHU and SADOWAY [25] detected four oxidation current peaks in anodic reaction and suggested the third current peak as the formation of graphite fluoride. Nevertheless, the electrode potential of C₂F₆ generation was not discussed. CHEN et al [26] observed different C-F bonds on the anode surface after electrolysis and considered this as an evidence of the existence of graphite fluoride. So far, more convincing evidence is needed to confirm the formation of graphite fluoride. The mechanism of PFC formation during aluminum reduction still deserves further investigation.

As for the formation mechanism of PFCs, at present, scholars mainly focus on experimental investigation, and theoretical exploration of micro formation mechanism is lacking. Therefore, in view of the unclear formation mechanism of PFCs and the lack of correlation between experiment and calculation, the combination of experiment and calculation is used to carry out the research. In this work, density functional theory (DFT) method is adopted to investigate the electrochemical reaction of fluorinated ions at the carbon anode/electrolyte interface [27,28]. The research experience in other fields shows that the chemical reaction process can be effectively simulated through molecular simulation and quantum chemical calculation, so as to describe the micro reaction process [29,30]. Meanwhile, laboratorial fluoride molten salt experiments are conducted to disclose electrode interface composition and bonding information. This work provides a theoretical basis for the source emission reduction of smelting pollutants in industrial production.

2 DFT calculation and experiments

2.1 Theoretical assumptions

The formation of PFCs in aluminum electrolysis is a complex electro-chemical process, simultaneously involving multiple reactants, electron transfer and high temperature. So far, no direct theoretical method capable of simulating such process has been established. To apply DFT method to this study, we have proposed two assumptions.

(1) The discharge of $[F]^-$ on anode could be divided into three processes: the migration of $[F]^-$ from the middle of electrolyte to the surface of anode, the electron transfer from $[F]^-$ to anode, and the occurrence of C — F interaction on anode surface.

(2) The electric potential of carbon anode surface equals everywhere in a very local microarea (atomic scale).

Through assumptions, it can be considered that the preponderant discharge position of $[F]^-$ on a very local anode surface could be estimated from the C—F bond energy.

2.2 Model structure

Pre-baked anode used in aluminum electrolysis is composed of multiple layers of irregularly stacked graphene. Consumption of carbon anode generally begins at the edges or surface defects of the monolayer of graphene. However, restricted by computation power, such complicated structure is hard to apply in quantum calculation. Hence, anode mode has been simplified in this study. The stack pattern of graphite layer is ignored given that it has little effect on chemical property of a very local structure.

Even though, several models should be investigated for their reactions in aluminum electrolysis. In this work, a typical single-layer small molecule aromatic fragment model (Model A) is used, as shown in Fig. 1(a). The C and H atoms related with reaction have been labeled for subsequent description, as shown in Fig. 1(b).

2.3 Calculation details

All DFT calculations were performed on the

Gaussian09D package [31]. All intermediates (IM) geometry optimization, frequency, and transition states (TS) were calculated at the B3LYP/6-311G++(d,p) level. Intermediates were confirmed with all real frequencies, and transition states were confirmed by only one imaginary frequency. Intrinsic reaction coordinate (IRC) [32] calculation was also employed to validate the connection between reactants and products. All energies reported herein were experienced by zero point energy (ZPE) correction.

To test the reliability of B3LYP/6-311G++(d,p), Model A was optimized at a variety of basis sets. The results are shown in Table 1.

From Table 1, it can be found that B3LYP/ 6-311G++(d,p), B3LYP/Def2-TZVP, M062x/ cc-pVTZ and CBS-QB3 show nearly the same results on describing the geometry of Model A.

The strength of C—F interaction at different sites on the anode was estimated by the bond energy. Single F atom was selected as the reference in order to deduce the absolute energy. The discharge priorities of different $[F]^-$ ions will be discussed in our following work. The C—F bond energy ($E_{\text{bond energy}}$) is given by Eq. (1):

 $E_{\text{bond energy}} = E_{\text{product}} - (E_{\text{F atom}} + E_{\text{reactant}}) \tag{1}$

where E_{product} is the total energy of C—F bonding product, $E_{\text{F atom}}$ is the energy of a fluorine atom, and E_{reactant} is the total energy of the reactant. Therefore, larger absolute value of $E_{\text{bond energy}}$ indicates stronger C—F bond.

In classical transition state theory, the reaction rate depends on the Gibbs free energy barrier (ΔG) at specific temperature. By comparing the Gibbs free energy barrier, the reaction rate can be qualitatively determined. On the basis of comparing the potential energy barrier ΔE at 0 K, we have further compared the Gibbs free energy barrier ΔG at 1250 K.

$$\Delta E = E_{\rm TS} - E_{\rm reactant} \tag{2}$$

$$\Delta G = G_{\rm TS} - G_{\rm reactant} \tag{3}$$

where the E_{TS} and G_{TS} are the potential energy and Gibbs free energy (1250 K) of transition state, respectively. E_{reactant} and G_{reactant} denote the potential energy and Gibbs free energy (1250 K) of reactant, respectively.

2.4 Molten salt experiment

High-purity graphite crucible was used as a reaction cell, and the reaction electrode was composed of high-purity graphite rod (Diameter d=5 mm). The bottom end of the exposed electrode



Fig. 1 Typical local edge structures of carbon anode Model A: (a) Schematic diagram of Model A; (b) Arrangement of C and H atoms in Model A

Bond	Bond angle/(°)	Bond length/Å			
		B3LYP/6-311++G(d,p)	B3LYP/Def2-TZVP	M062x/cc-pVTZ	CBS-QB3
$C_1 - C_2$	120.78	1.391	1.387	1.384	1.390
$C_2 - C_3$	120.77	1.417	1.414	1.411	1.417
C ₃ -C ₁₃	120.74	1.429	1.426	1.421	1.429
C_1 — H_1	120.79	1.085	1.083	1.082	1.084

Table 1 Bond length and angle in Model A

was dipped into the molten salt and used as the reaction interface. 550 g of uniform reactant mixture which consists of NaF (54.8 wt.%) + AlF_3 $(44.7 \text{ wt.\%}) + \text{Al}_2\text{O}_3$ (0.5 wt.\%) was used as the electrolyte. Alumina was analytically pure and cryolite was synthetic one. The required reagent was placed in a drying oven to dry for 24 h before the experiment. A self-made well furnace equipped with a CW-3100 temperature controller and an MPS705 DC (0-60 V and 0-20 A) steady current and voltage supply was used. The electrolysis temperature was 1250 K. The constant current was 1.5 A/cm². The electrolysis duration was 2 h. The anode was removed from the electrolyte before electricity black-out to minimize the adhesion of the electrolyte to the surface of the anode. The surface of the electrolyzed graphite anode was cut after air cooling. The sample surface was analyzed by X-ray photoelectron spectroscopy (XPS), in order to obtain the chemical valence states of each element.

3 Results and discussion

3.1 Quantum chemical calculation results

3.1.1 Initial reaction steps of Model A

Prior to the illustration of PFC formation, the

reactions related with H atoms in Model A need to be illustrated. The C—F bond energies at different positions have been calculated to evaluate the discharge sequence of $[F]^-$ in Model A. Results are shown in Table 2.

Table 2 Potential energy ΔE and Gibbs free energy change ΔG (1250 K) of C—F bond at different positions

<u> </u>	,	1
Position	$\Delta E/(\mathrm{kJ}\cdot\mathrm{mol}^{-1})$	$\Delta G/(\text{kJ}\cdot\text{mol}^{-1})$
C_1 —F	-285.60	-125.65
C_2 —F	-285.56	-125.56
C ₁₃ —F	-112.21	47.45

From Table 2, it can be seen that both the ΔE and ΔG (1250 K) of C—F bond at C₁ site are much lower than those at other sites. This indicates that $[F]^-$ is more likely to discharge and form anode chemically absorbed F (F_{anode}) at the edge of aromatic fragment. Elimination of H atom is through combination with F_{anode} . Potential energy surface (PES) of the H atom elimination process is shown in Fig. 2. The energy above the horizontal line represents the relative energy at 0 K, and the energy in brackets below the horizontal line is the relative energy at 1250 K.

For the process of Original to I3, [F]⁻ discharges



Fig. 2 PES of H atom elimination process

at C₁ and C₂ positions stepwise, leading to formation of $C_1 - F_1$ and $C_2 - F_2$ bonds, respectively. Following, the interaction of F atom (C_1 position) with the H atom (C_2 position) gives a HF molecule and thus leads to I3 intermediate. The potential energy barrier of the HF formation from I2 is 210.83 kJ/mol. Subsequently, [F]⁻ discharges on the newly generated I3 structure to form I5 at C1 and C_{12} positions stepwise, which could be transformed to I6 and HF via C₁-F interaction accompanied with C_{12} — H_3 bond cleavage and F— H_3 bond formation. The potential energy barrier of this process is 115.65 kJ/mol. Likewise, the reaction of I6-I9 is analogy to RE-I5 process. The potential energy barrier of the HF formation from I8 is 190.29 kJ/mol. Thus, the original H atoms are replaced by F bonds through six [F]⁻ discharges. $3.1.2 \text{ CF}_x$ formation

For intermediate I9, the discharge of $[F]^-$ would lead to ring opening and thus three $-CF_x$ chain groups are generated. Details of this process are demonstrated in Fig. 3.

The stepwise discharge of $[F]^-$ at C₂, C₁₂, C₁ and C₁₁ positions leads to the formation of C₂—F₁, C₁₂—F₂, C₁—F₃ and C₁₁—F₄ bonds, respectively. Three ring opening pathways for IM3 have been identified. Via transition state TS4, IM4 is obtained through C_1-C_{12} bond cleavage. The opening of the six-carbon ring leads to a $-C_2F_5$ chain. The potential energy barrier of this process at 0 K is 382.17 kJ/mol, and Gibbs free energy barrier at 1250 K is 367.82 kJ/mol. Besides, IM5 is converted from IM3 via transition state TS5 by overcoming a potential energy barrier of 361.37 kJ/mol (Gibbs free energy barrier is 345.01 kJ/mol). The ring opening causes the formation of $-C_3H_7$ group. Additionally, IM3 could transform to IM6 via transition state TS4 by $C_{11}-C_{12}$ bond cleavage, resulting in another $-C_3H_7$ group. The potential energy barrier of this process is 348.11 kJ/mol (Gibbs free energy barrier of this process is 348.11 kJ/mol (Gibbs free energy barrier is 1146.92 kJ/mol).

It can be deduced that the formation of IM6 is favored over other intermediates by comparing potential energies. However, when the temperature rises to 1250 K, the Gibbs free energy barrier of IM6 is the largest, which is difficult to generate. Relatively speaking, IM4 is very thermodynamically stable. The three intermediates are supposed to co-exist during PFC formation. In the following, the PFC formation from IM4, IM5 and IM6 will be discussed.

3.1.3 PFC formation from IM5 and IM6

IM5 could be converted into IM10 and undergo 8 pathways. Details of these pathways have



Fig. 3 PES of I9 reactions

been illustrated in Fig. 4 and Fig. 5. For IM6 and IM5 pathways cross at IM10 intermediate, Fig. 4 also contains the reaction pathway of IM6. The PES of $Pro1 + CF_4$ and $Pro2 + C_2F_6$ formation pathways can be found in Fig. 4.

IM10 can be converted from IM5 by discharge of two $[F]^-$ anions at C_{11} position, leading to C_{11} — F_1 and C_{11} — F_2 bond formation. Alternatively, IM10 can also be generated from IM6. Specifically, the $[F]^-$ discharge at C_{12} position of IM6 forms IM7. Following, IM8 is formed from IM7 by C_{12} —F bond crack and C_{11} —F bond formation via TS7 (The potential energy barrier is 508.19 kJ/mol). Another $[F]^-$ discharge at C_{12} site of IM8 forms IM10. Considering the potential energy barrier in IM6–IM10 pathway, pathway of IM5–IM10 is considered to be favored.

Pro1 + CF₄ can be formed from IM10 by C_{12} — C_1 , C_{11} — F_1 bond cleavage and C_{12} — F_1 bond formation via transition state TS8. The potential energy barrier is 438.02 kJ/mol. Meanwhile, Pro2 + C_2F_6 can be produced from IM10 via transition state TS9 through C_1 — C_2 and C_{11} — F_2 cleavage accompanied with C_1 — F_2 formation. The potential energy barrier is 390.20 kJ/mol.

IM9 and IM10 could undergo additional pathways to form anther four products. Details can be found in Fig. 5.

The discharge of $[F]^-$ at C_{10} site of IM9 forms IM10, as shown in Fig. 4. Whereas, the [F]⁻ discharge at C₁₃ position of IM9 forms IM13. From IM13, two possible intermediates, IM14 and IM15, could be formed via $[F]^-$ discharge at C₃ and C₁₃ positions. Three possible pathways for IM14 to generate PFC have been found. The first path is the cleavage of C1-C12, forming -CF3 group. The interaction of F atom (C_{13} position) with the $-CF_3$ group gives a CF₄ molecule and thus leads to product Pro4. The second path is the cleavage of C_2 — C_3 , resulting in — C_3F_7 group. The interaction of F atom (C₂ position) with the $-C_3F_7$ group forms a C₃F₈ molecule and thus leads to Pro5. The third path is to convert to IM16 via [F]⁻ discharge at C_{12} site. The following cleavage of C_1 — C_2 forms $-C_2F_5$ group. Pro6 (C₂F₆) is produced through the elimination of F atom (C_1 position) with the $-C_2F_5$ group.

For IM15, two possible reaction paths have been identified. Via transition state TS10, $Pro3 + CF_4$ is generated by $C_1 - C_{12}$ and $C_{13} - F_1$



Fig. 4 PES of IM5 and IM6 reaction pathways

cleavage accompanied with C_{12} — F_1 formation. The potential energy barrier of this step is 415.68 kJ/mol. Additionally, $[F]^-$ discharge at C_3 position of IM15 forms IM12. Then, IM12 dissociates to Pro6 + C_2F_6 via TS13 by C_1 — C_2 and C_{13} — F_2 cleavage accompanied with C_1 — F_2 formation. The potential energy barrier is 418.73 kJ/mol.

There are five possible paths to produce the final product, the potential energy barrier appears in the process of forming $-CF_3$, $-C_2F_5$ and $-C_3F_7$ groups. The maximum potential barrier and maximum Gibbs free energy barrier of each pathway are listed in Table 3. It can be seen that $Pro5 + C_3F_8$ is relatively easy to be generated.

3.1.4 IM4 reaction process

PES of the reaction path of IM4 is shown in Fig. 6.

The discharge of $[F]^-$ at C₃ and C₁₃ sites of IM4 results in IM20. Depending on the discharge sequence of C₃ and C₁₃ sites, two competitive intermediates, IM17 and IM18, could be converted. Judging from the potential energy and the Gibbs free energy, IM18 is more favorable than IM17. Via transition state TS17, Pro7 + C₂F₆ can be formed through $-C_2F_5$ group combining with the additional absorbed F atom. The potential energy barrier of this process is 238.24 kJ/mol.

Notably, two intermediates, IM21 and IM22, could be formed in IM4 reactions. Besides, there are two possible paths to produce IM21. Firstly, the discharge of $[F]^-$ at C₁₃ forms IM18, which could be converted to IM21 via TS16 by F atom migration from C₁₃ to C₁₂ site. The potential energy barrier of this step is 77.15 kJ/mol. In the other route, IM21



Fig. 5 PES of IM9 reaction pathways

Table 3 Maximum potential energy barrier $\Delta_{\max}E$ and Gibbs free energy barrier $\Delta_{\max}G$ (1250 K) of IM9 reaction pathways

Final product	Reaction path	$\Delta_{\max} E/(kJ \cdot mol^{-1})$	$\Delta_{\max}G/(\mathrm{kJ}\cdot\mathrm{mol}^{-1})$
Pro3+CF ₄	$IM9 \rightarrow IM13 \rightarrow IM15 \rightarrow TS10 \rightarrow Pro3 + CF_4$	415.68	403.71
Pro4+CF ₄	$IM9 \rightarrow IM13 \rightarrow IM14 \rightarrow TS11 \rightarrow Pro4 + CF_4$	348.15	333.00
Pro5+C ₃ F ₈	$IM9 \rightarrow IM13 \rightarrow IM14 \rightarrow TS12 \rightarrow Pro5 + C_3F_8$	190.87	182.51
	$IM9 \rightarrow IM13 \rightarrow IM14 \rightarrow IM16 \rightarrow TS14 \rightarrow Pro6 + C_2F_6$	435.01	358.69
$Proo+C_2F_6$	$IM9 \rightarrow IM13 \rightarrow IM15 \rightarrow IM12 \rightarrow TS13 \rightarrow Pro6 + C_2F_6$	418.73	339.07



Fig. 6 PES of IM4 pathways

is formed by IM19 via TS15 by F atom migration. The potential energy barrier is 151.88 kJ/mol. There are also two possible paths to form IM22. IM22 is converted from IM20 via transition state TS18 by the migration of F from C_{13} site to C_{12} site. The potential energy barrier is 238.24 kJ/mol. IM22 could also be generated from IM21 by $[F]^-$ discharge at C_3 site. PES of IM21 reaction pathways are illustrated in Fig. 7.

Three possible paths for further reaction of IM21 have been found. Pro8 + CF₄ is generated from IM21 via transition state TS19 through C_1 — C_2 and C_{12} — F_1 cleavage accompanied with $C_{13} - F_1$ and $C_2 - C_3$ formation. The potential energy barrier is 514.63 kJ/mol. The second path is via the discharge of $[F]^-$ at C_1 and C_{13} positions of IM21, leading to the formation of IM23 and IM25 stepwise. Then, the cleavage of C₁₂-C₁₁ gives a $-CF_3$ group and the interaction of F atom (C₁₃ position) with the $-CF_3$ group forms a CF_4 molecule. The potential energy barrier is 220.83 kJ/mol. The third path is via the stepwise discharge of $[F]^-$ at C₃ and C₁₃ sites, leading to the formation of IM22 and IM24, respectively. Finally, the cleavage of C₂-C₃ bond causes ring opening and thus forms a -C₂F₅ group. Interaction of F atom (C_{13} position) with the $-C_2F_5$ group gives a C_2F_6 molecule. The potential energy barrier is 181.33 kJ/mol.

For the three reaction paths, the energy barrier appears in the process of forming $-CF_3$ or $-C_2F_5$ group, therefore, the elimination step of $-CF_3$ or $-C_2F_5$ is the rate-limiting step. From the aspect of the Gibbs free energy barrier, the third reaction pathway is more likely to take place.

3.1.5 Further reactions of Pro8 and Pro10

We have also found that the products above possibly undergo further reactions by $[F]^-$ discharge. In this section, further reactions of Pro8 and Pro10 will be discussed. PES of IM8 reaction path is presented in Fig. 8.

Firstly, $[F]^-$ discharges at C₁ position of Pro8, leading to the formation of C₁₁—F bond. Then, Pro8 transforms into IM26. IM27 can be produced from IM26 via transition state TS22 through C₂—C₁₂ and C₁₁—F cleavage accompanied with C₁₂—F formation. The potential energy barrier is 349.95 kJ/mol. Then, $[F]^-$ discharges at C₂, C₁₁ and C₃ positions stepwise to form IM28, IM29 and IM30. IM31 is generated through C₃—F₁ cleavage accompanied with C₁₃—F₁ formation via transition state TS23. The potential energy barrier is 55.48 kJ/mol. Subsequently, the cleavage of C₁₂—C11 bond forms a —CF₃ group. Finally, CF₄



Fig. 7 PES of IM21 pathways



Fig. 8 PES of Pro8 transforming into product Pro10 + CF₄

is obtained via the interaction of F atom (C_{13} position) with the $-CF_3$ group. The potential energy barrier is 221.63 kJ/mol.

From Pro8 to $Pro10 + CF_4$, the highest potential energy barrier is 349.95 kJ/mol in the IM26–IM27 process. It shows that the decisive step

in the whole reaction process is the opening of carbon ring caused by the cleavage of C—C bond.

 $Pro5 + C_2F_6$ could also be produced from Pro8. The PES of reaction path is shown in Fig. 9.

IM26 can be formed from Pro8 via [F]⁻ discharge at C₁ position. IM32 is then converted via transition state TS25 through carbon ring opening at $C_{12} - C_{11}$. The potential energy barrier of this process is 130.25 kJ/mol. The following discharge of $[F]^-$ at C_{11} position forms IM33. IM34 is produced via transition state TS26 through C₁₁-F cleavage accompanied with $C_1 - F$ formation. The potential energy barrier is 1.88 kJ/mol. Subsequently, $[F]^-$ discharges at C_{13} and C_3 positions and thus forms IM35 and IM36. The cleavage of C₂-C₃ bond of IM36 generates a $-C_2F_5$ group. Through F atom (C₁₃ position) interaction with the $-C_2F_5$ group, C_2F_6 is finally The potential energy produced. barrier is 203.26 kJ/mol.

From Pro8 to Pro5 + C_2F_6 , the highest potential energy barrier is 203.26 kJ/mol in the process from IM36 to Pro5 + C_2F_6 . It shows that the speed determining rate step in the whole reaction process is the breaking of C—C bond, resulting in the stripping of $-C_2F_5$ group.

Another pathway for IM26 is shown in Fig. 10.

By two the discharge of $[F]^-$ at C₁₃ and C₃ sites of Pro10, IM38 can be converted. Pro5 + CF₄ is then formed via transition state TS28 by the elimination of —CF₃ with another F atom. The potential energy barrier of this step is 222.84 kJ/mol.

It is suggested that the three H atoms connected to the three C atoms (C₁, C₂ and C₁₂) of benzene ring are firstly substituted by F atom and then saturated by chemically absorbed F atom, and finally transformed into $-C_xF_y$ group via ring opening. CF₄ and C₂F₆ molecules are formed via the elimination of $-C_xF_y$ group with additional chemically absorbed F atom. Hence, PFC formation needs multiple F atom participation.

3.2 Molten salt experiment results

The high-resolution C 1s and F 1s XPS spectra of Sample A were fitted and analyzed by Thermo Avantage software to obtain the detailed chemical valence and structure information of the anode surface. The fitting results are shown in Fig. 11.

It can be seen from Fig. 11(a) that the C 1s contains 7 component peaks. The two strongest component peaks C_1 and C_2 are C sp², which is the main component in graphite, with a binding energy of 284.45 and 284.72 eV, respectively. C_3 , with a binding energy of 284.82 eV, is C sp³ that can be



Fig. 9 PES of Pro8 transforming into product $Pro5 + C_2F_6$



Fig. 10 PES of Pro10 pathway



Fig. 11 High-resolution C 1s (a) and F 1s (b) XPS spectra of Sample A

assigned to a nonfunctional graphite aromatic ring. The binding energies of C_4 and C_5 peak sites are 285.62 and 285.91 eV, which should be corresponding to the C—O and C—H structures, respectively. C 1s peaks with binding energies higher than 289 eV are fluorinated covalent C—F bond (C_6) and ionic C—F bond (C_7). The F 1s also contains 6 component peaks (Fig. 11(b)). Except for the NaF component peak of F₁ with binding energy of 684.77 eV, the other five component peaks are all C — F bonds. The F₂ with binding energy of 685.82 eV is ionic C—F bond [33]. The binding energies of F₃ and F₄ at 686.57 and 687.13 eV represent the semi-ionic C—F bond, respectively. F₅, which has a binding energy of 688.33 eV, is a covalent C—F bond. The content of F₅ is very low. The binding energy of F₆ is 690.90 eV, which indicates a —CF₂ structure.

By adjusting the voltage to induce anode effect in molten salt electrolysis experiment, the composition and relative content of F element in each chemical state of Sample A were analyzed. It was found that when the anodic potential reached the $[F]^-$ discharge potential, C-F bonds that represent different structural forms were detected on the anodic surface after electrolysis, and there were semi-ionic C-F bond, ionic C-F bond, covalent C - F bond, and $- CF_2$ bond. The proportion of C—F bond in Sample A is roughly: ionic C-F bond (42.73%), semi-ionic C-F bond (24.7%), covalent C—F bond (1.69%), and $-CF_2$ (7.77%). After electrolysis, C-F bonds of different structural forms were detected on the anode surface, which is in accordance with the results of first-principles calculations. This proves that there would be different forms of C-F bonds generated during the process of [F]⁻ discharge. The [F]⁻ will continue to discharge on the anode surface, and eventually break the bond to form the products CF₄ and C₂F₆.

4 Conclusions

(1) The discharge of fluorine containing anions ([F]⁻) on carbon anode may lead to the saturation of aromatic rings, resulting in the formation of $-CF_3$ or $-C_2F_5$ groups via ring opening. The subsequent elimination of $-CF_x$ groups with additional F atom can generate PFC.

(2) Compared with CF_4 formation, higher potential energy barrier and Gibbs free energy barrier have been located in C_2F_6 formation path. It is partially indicated that CF_4 is favored in aluminum electrolysis exhaust, which is consistent with industry situation. However, more structure models are needed to be investigated in following work.

(3) The XPS analysis indicates that different -CF and $-CF_2$ exist on the carbon anode surface after laboratorial electrolysis. This is in good

1716

agreement with the DFT calculations that PFC could be directly converted from $-CF_x$ groups.

Acknowledgments

The authors are grateful for the financial supports from the National Natural Science Foundation of China (Nos. 51974373, 51874365, 62133016), the Major Scientific and Technological Innovation Projects of Shandong Province, China (No. 2019JZZY020123), and the Fundamental Research Funds for the Central Universities of Central South University, China (No. 2019zzts242).

References

- DION L, MARKS J, KISS L I, PONCSÁK S, LAGACÉ C L. Quantification of perfluorocarbons emissions during high voltage anode effects using non-linear approach [J]. Journal of Cleaner Production, 2017, 164: 357–366.
- [2] YANG Shuai, ZHANG Hong-liang, ZOU Zhong, LI Jie, ZHONG Xiao-chong. Reducing PFCs with local anode effect detection and independently controlled feeders in aluminum reduction cells [J]. JOM, 2020, 72(1): 229–238.
- [3] SAEVARSDOTTIR G, KVANDE H, WELCH B J. Aluminum production in the times of climate change: The global challenge to reduce the carbon footprint and prevent carbon leakage [J]. JOM, 2020, 72(1): 296–308.
- [4] BURKAT V S, ZOR'KO K I, BOZHKO A G, SPIRIN A V, REBRIK I I, VASIN S Y. Study of perfluorocarbon release during aluminum production in vertical-stud electrolytic cells with self-baking anode in between anode effects [J]. Metallurgist, 2019, 63(1/2): 192–196.
- [5] DION L, GABOURY S, PICARD F, KISS L I, PONCSAK S, MORAIS N. Universal approach to estimate perfluorocarbons emissions during individual high-voltage anode effect for prebaked cell technologies [J]. JOM, 2018, 70(9): 1887–1892.
- [6] THONSTAD J, ROLSETH S, CHEMISTRY S M A. Low voltage PFC emission from aluminium cells [J]. Journal of Siberian Federal University – Chemistry, 2017, 10(1): 30–36.
- [7] TAN M, LI T, SHANG B, CUI H N. Quantum chemical prediction of the spectroscopic properties and ionic composition of the molten NaF–AlF₃ salts [J]. Journal of Molecular Liquids, 2020, 317: 113937.
- [8] GUO Hui, LI Jie, ZHANG Hong-liang, LUO Jia-wei, WANG Jing-kun, MOU Chun-ling, WU Shang-yuan, ZONG Chuan-xin. Study on micro-structure and transport properties of KF–NaF–AlF₃–Al₂O₃ system by first-principles molecular dynamics simulation [J]. Journal of Fluorine Chemistry, 2020, 235: 109546.
- [9] STANIC N, EMBLA T B, SANDNES E. CO and CO₂ anode gas concentration at lower current densities in cryolite melt [J]. Metals, 2020, 10(12): 1694.
- [10] ZHANG Ming-jie, QIU Zhu-xian, WANG Hong-kuan. Electrode process in aluminum electrolysis—I. Anode

process [J]. Journal of Northeastern University (Natural Science), 2001, 22(2): 8–11. (in Chinese)

- [11] DANDO N R, SYLVAIN L, FLECKENSTEIN J, KATO C, SON V V, COLEMAN L. Sustainable anode effect based perfluorocarbon emission reduction [C]//Light Metals 2011. San Diego, CA: TMS, 2011: 325–328.
- [12] MARKS J, TABEREAUX A, PAPE D, BAKSHI V, DOLIN E J. Factors affecting PFC emissions from commercial aluminum reduction cells [C]//Light Metals 2001. New Orleans, LA: TMS, 2001: 295–302.
- [13] VOGT H. On the mechanism of the anode effect in aluminum electrolysis [J]. Metallurgical and Materials Transactions B, 2000, 31(6): 1225–1230.
- [14] THONSTAD J, NORDMO F, VEE K. On the anode effect in cryolite-alumina melts—I [J]. Electrochimica Acta, 1973, 18(1): 27–32.
- [15] KIM J, FRASER P J, LI S L, ET A L. Quantifying aluminum and semiconductor industry perfluorocarbon emissions from atmospheric measurements [J]. Geophysical Research Letters, 2014, 41(13): 4787–4794.
- [16] ZHU Hong-min, SADOWAY D R. An electroanalytical study of electrode reactions on carbon anodes during electrolytic production of aluminum [C]//Light Metals 2000. Warrendale, PA: TMS, 2000: 257–263.
- [17] LEBER B P, TABEREAUX A T, MARKS J, LAMB B, HOWARD T, KANTAMANENI R, GIBBS M, BAKSHI V, DOLIN E J. Perfluorocarbon (PFC) generation at primary aluminum smelters [C]//Light Metals 1998. San Antonio, TX: TMS, 1998: 1015–1023.
- [18] MARKS J, KANTAMANENI R, PAPE D, RAND S. Protocol for measurement of tetrafluoromethane and hexafluoroethane from primary aluminum production [C]//Light Metals 2013. San Antonio, TX: TMS, 2013: 1032–1036.
- [19] MARKS J, BAYLISS C. GHG measurement and inventory for aluminum production [C]//Light Metals 2012. Orlando, FL: TMS, 2012: 805–808.
- [20] WONG D S, MARKS J. Continuous PFC emissions measured on individual 400 kA cells [C]//Light Metals 2013. San Antonio, TX: TMS, 2013: 865–870.
- [21] TABEREAUX A T. Anode effects, PFCs, global warming, and the aluminum industry [J]. JOM, 1994, 46(11): 30–34.
- [22] NISSEN S S, SADOWAY D R. Perfluorocarbon (PFC) generation in laboratory-scale aluminum reduction cells [C]//Light Metals 1997. Nashville, TN: TMS, 1997: 159–164.
- [23] QIN Qing-dong, CHAI Deng-peng, QIU Shi-lin, LUO Li-fen. Study on PFC emission characteristics of 300 kA aluminium electrolysis cells [J]. Light Metals, 2012(1): 27–31. (in Chinese)
- [24] QIN Qing-dong, QIU Shi-lin. Study on the mechanism of PFC emission during the industrial aluminum electrolysis process [J]. Light Metals, 2015(6): 23–27. (in Chinese)
- [25] ZHU H M, SADOWAY D R. Towards elimination of anode effect and PFC emissions via current shunting [C]//Light Metals 2001. New Orleans, LA: TMS, 2001: 303–306.
- [26] CHEN Gong, SHI Zhong-ning, GAO Bing-liang, HU Xian-wei, WANG Zhao-wen. Electrochemical behavior of

graphite anode during anode effect in cryolite molten salts [J]. Transactions of Nonferrous Metals Society of China, 2012, 22(9): 2306–2311.

- [27] KOLB M J, CALLE-VALLEJO F, JUURLINK L B F, KOPER M T M. Density functional theory study of adsorption of H₂O, H, O, and OH on stepped platinum surfaces [J]. Journal of Chemical Physics, 2014, 140(13): 134708.
- [28] CRISPIN X, GESKIN V M, BUREAU C, LAZZARONI R, SCHMICKLER W, BRÉDAS J L. A density functional model for tuning the charge transfer between a transition metal electrode and a chemisorbed molecule via the electrode potential [J]. The Journal of Chemical Physics, 2001, 115(22): 10493–10499.
- [29] WU Hong-fei, CHEN Chao-yi, LI Jun-qi, LAN Yuan-pei, WANG Lin-zhu, QUAN Bian-li, JIN Hui-xin. A density functional model for tuning the charge transfer between a transition metal electrode and a chemisorbed molecule via the electrode potential [J]. Transactions of Nonferrous Metals

Society of China, 2020, 30(6): 1662–1673.

- [30] ZHU Guang-li, WANG Yu-hua, WANG Xu-ming, MILLER J D, LU Dong-fang, ZHENG Xia-yu, ZHAO Yue-hao, ZHENG Hai-tao. Effects of grinding environment and lattice impurities on spodumene flotation [J]. Transactions of Nonferrous Metals Society of China, 2019, 29(7): 1527–1537.
- [31] FRISCH M J, TRUCKS G W, SCHLEGEL H B, SCUSERIA G E, ROBB M A, CHEESEMAN J R, SCALMANI G, BARONE V, MENNUCCI B, PETERSSON G A, NAKATSUJI H. Gaussian 09 [M]. Wallingford: Gaussian, Inc, CT, 2009.
- [32] GONZALEZ C, SCHLEGEL H B. Reaction path following in mass-weighted internal coordinates [J]. The Journal of Physical Chemistry, 1990, 94: 5523–5527.
- [33] MOULDER J F. The impact of the scanning XPS microprobe on industrial applications of X-ray photoelectron spectroscopy [J]. Journal of Electron Spectroscopy and Related Phenomena, 2019, 231: 43–49.

铝电解全氟化碳气体的微观形成机理

孙珂娜^{1,2},李劼^{1,2},张红亮^{1,2},李天爽^{1,2}

1. 中南大学 冶金与环境学院,长沙 410083;
2. 中南大学 低碳有色冶金国家工程研究中心,长沙 410083

摘 要:针对目前铝电解阳极效应阶段全氟化碳(PFCs)气体排放原因不明的问题,采用密度泛函理论计算与 X 射 线光电子能谱(XPS)检测手段对 PFCs 的微观形成机理进行研究。计算结果表明,在阳极表面不断放电的过程中, 熔盐中含氟配离子[F]⁻使碳环边缘的 C一H 键逐渐被 C一F 键取代,导致芳香族 C一C 键饱和,随后碳环开环逐渐 形成一CF₃基团和一C₂F₅基团,最终脱出 CF₄和 C₂F₆产物。XPS 结果表明,电解后的阳极表面存在不同类型的一 CF_x结构,验证了量子力学计算中[F]⁻在碳边缘不断放电、最终形成不同 C一F 键的可能性。 关键词:微观形成机理;铝电解;全氟化碳气体;密度泛函数理论计算

(Edited by Wei-ping CHEN)