

Electrochemical behavior of Li incorporation in Al in LiTFSI/KTf molten salt electrolyte

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Abstract: The electrochemical behavior of lithium incorporated in aluminum electrode in LiTFSI/KTf (lithium bis (trifluoromethylsulfonyl) amide/CF₃SO₃K) molten salt electrolyte was studied by a variety of electrochemical techniques including cyclic voltammetry, chronopotentiometry and chronoamperometry. The reduction reaction is found involving a nucleation process on the aluminum electrode. The results of chronopotentiometry indicate that the process of lithium incorporation in aluminum is smooth and uniform. The galvanostatic cycle experiments show that the coulombic efficiency is very low in the first cycle, which is mainly due to the “retention capacity” of Li–Al alloys. This characteristic is testified by the results of XRD and SEM. The results of chronoamperometry indicate that the incorporation of lithium into aluminum for the formation of α -phase Li–Al alloy is limited by its diffusion rate, with a measured diffusion coefficient of 1.8×10^{-10} cm²/s.

Key words: molten salt; aluminum electrode; cyclic voltammetry; coulombic efficiency; nucleation process

1 Introduction

Molten salts which consist of cations and anions are normally free of any solvents as electrolytes. They differ from the classic solutions of electrolyte due to the special systems which lead to the excellent characteristics such as low vapor pressure, nonflammability, high ionic conductivity and large electrochemical window [1–3]. Molten salts could be simply classified into three groups by the operating temperature range, high temperature molten salts ($t > 400$ °C), intermediate temperature molten salts (100 °C $< t < 400$ °C) and low temperature (room temperature) molten salts ($t < 100$ °C). These three types of molten salt electrolytes have their own application fields of electrochemical devices because of the difference between the physicochemical properties (melting temperature, thermal stability, ionic conductivity, etc.).

Application of high temperature molten salts in high temperature lithium batteries (HTLBs, also called as

lithium thermal batteries) is one of the representative cases. The HTLBs have long been used for military purposes [4–7]. They are reliable, rugged and robust. Recently, the application of HTLBs for geothermal and oil/gas borehole power sources is increasingly attracting the attention. The goal is to use the heat of borehole to keep the electrolytes in the molten state, thus the use of internal pyrotechnic systems of the HTLBs can be eliminated. However, this would require the electrolytes which melt and keep thermal stability at the intermediate temperatures, especially under 300 °C [3,5]. In this frame, the traditional alkali metal halides, belonging to the high temperature molten salts, such as LiCl–KCl [8,9] and LiF–LiCl–LiBr [5], cannot be applied in HTLBs in the absence of the internal pyrotechnic systems due to their high melting points. Thus, investigations in the fields of new molten salt electrolytes have seen tremendous increase in popularity. Introduction of the Cs and Rb cations into the alkali halide electrolytes seemed to be a beneficial attempt and was expected to lower the melting temperatures;

however, the high cost of the Cs and Rb halides made them unattractive with commercialization [3]. The iodide-based electrolytes [7,10,11], which possess low melting points, could be considered a promising alternative; however, the issues of high cost, sensitivity toward oxidation by oxygen and hygroscopic character, may limit the commercial manufacturing [3,5]. Compared with the alkali halide electrolytes, the nitrate-based electrolytes appear to be promising for use as electrolytes in HTLBs because of their much lower melting points, but the protective passivation layer of Li_2O would be disrupted when the operating temperature is elevated to a certain value, which would result in unacceptable hazards to the battery and the nearby equipments [12].

Thus, investigations in the fields of novel electrolytes which melt under $300\text{ }^\circ\text{C}$ are of great importance for HTLBs as geothermal and oil/gas borehole power sources. A number of organics with low melting points are potential candidates for HTLBs and some of which have been studied for possible applications in HTLBs [3,5]. The bis (trifluoromethylsulfonyl) amide (TFSI) anion is well-known as one of the major anions producing molten salt electrolytes with low melting points [13–19]. MA et al [20] have previously reported a molten salt electrolyte based on the LiTFSI and $\text{CF}_3\text{SO}_3\text{K}$ (KTf). The LiTFSI/KTf mixture, at the molar ratio of 1:1, has the eutectic temperature of $160\text{ }^\circ\text{C}$ and could be thermally stable under $300\text{ }^\circ\text{C}$. This mixture was expected to be used at intermediate temperatures. The present work is concerned with the investigation of the electrochemical behavior of lithium incorporated into aluminum in the LiTFSI/KTf molten salt electrolyte at $240\text{ }^\circ\text{C}$ (as Li–Al alloys are commonly used as anodes in HTLBs, we estimated the ability of the LiTFSI/KTf molten salt to be used as the electrolyte with Al working electrode). A variety of electrochemical techniques are used including cyclic voltammetry, chronopotentiometry and chronoamperometry. The morphology, and crystal structure of the fresh Al and electrochemically formed Li–Al alloy are characterized by scanning electron microscopy (SEM) and X-ray diffraction (XRD), respectively.

2 Experimental

The preparation of the LiTFSI/KTf molten salt electrolyte at the molar ratio of 1:1 has been described elsewhere [20]. The working electrode was an aluminum wire with a high purity (99.99%) and a diameter of 1.38 mm. In some experiments, the aluminum foil (99.999% pure) was used as the working electrode which had an area of 1 cm^2 exposed to the LiTFSI/KTf molten salt electrolyte. The spectroscopically pure graphite rod was

used as the counter electrode. The platinum wire with a diameter of 0.3 mm was used as the pseudo-reference electrode. The potential of this electrode was calibrated with the Li/Li^+ dynamic electrode. Detailed information about the preparation of the Li/Li^+ dynamic electrode can be found in Ref. [21]. All potentials given in this work are referred to this Li/Li^+ dynamic potential.

The cyclic voltammetry, chronopotentiometry and chronoamperometry experiments were carried out with an AutoLab PGSTAT 30 electrochemical workstation in a homemade experimental apparatus, as presented in Fig. 1. The cyclic voltammetry was conducted in the potential range of 3–0 V at a scan rate of 100 mV/s . The chronoamperometry experiments were performed at the potentials of 150, 125, 100, 75 and 50 mV, and the current densities of 1.0, 2.5 and 5.0 mA/cm^2 were employed for the galvanostatic deposition and stripping of Li measurements. All electrochemical measurements were carried out under argon atmosphere.

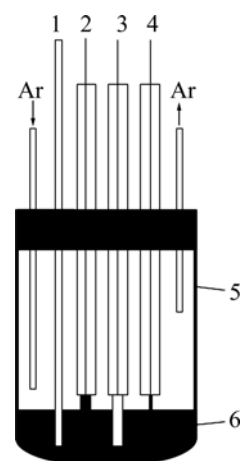


Fig. 1 Schematic representation of experimental apparatus for electrochemical measurements: 1—Thermocouple; 2—Counter electrode (spectroscopically pure graphite rod); 3—Working electrode (aluminum wire or aluminum foil); 4— Pseudo-reference electrode (calibrated with Li/Li^+ dynamic electrode); 5—Pyrex cell; 6—LiTFSI/KTf molten salt electrolyte

The morphologies of the fresh Al and the electrochemically formed Li–Al alloy were determined by SEM (Hitachi S–4700), using $\text{Cu K}\alpha$ radiation. X-ray diffraction was carried out with a Thermo ARL SCINTAG X’TRA at room temperature, using a $\text{Cu K}\alpha$ radiation source under the voltage of 45 kV and the current of 40 mA. The XRD patterns were recorded with the step size of 0.04° at the speed of $2.4\text{ }^\circ/\text{min}$.

3 Results and discussion

3.1 Cyclic voltammetry

Figure 2 shows a typical cyclic voltammogram of the reduction/oxidation reaction of lithium on the

aluminum electrode, recorded at a scan rate of 100 mV/s at 240 °C. During the forward sweep, current starts increasing at about 0.25 V which could be ascribed to the reduction of Li^+ and resulted in the formation of Li–Al alloy. As seen from Fig. 2, a remarkable feature is the appearance of a hysteresis in the cathodic current when the direction of sweep was reversed, which could be attributed to a nucleation process of crystal growth [22]. There is no second oxidation peak in the anodic current. It differs from the previously reported result that three couples of oxidation/reduction reversible peaks could be observed for the aluminum electrode in the alkali metal halide melts and each couple of reversible peaks were associated to a Li–Al alloy phase transition [23–25]. Therefore, it is considered that only one of the Li–Al phases is reversible for aluminum electrode in LiTFSI/KTf molten salt. The cyclic voltammetry is regarded as a semi-quantitative tool and can be considered a rapid charge–discharge cycle. Thus, the efficiency of lithium recoveries could be calculated to be about 85% based on the rapid charge–discharge cycle, and arrived at a constant value of about 95% after several cycles.

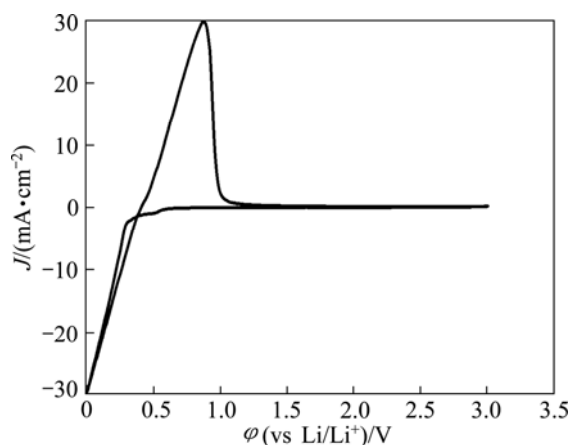


Fig. 2 Cyclic voltammogram of aluminum electrode in LiTFSI/KTf molten salt electrolyte at 240 °C and 100 mV/s

3.2 Coulombic efficiency

From a battery viewpoint, the technique of charge–discharge cycles at constant current densities is probably a better one to check the electrochemical performance of aluminum in LiTFSI/KTf molten salt electrolyte. A typical chronopotentiometric curve recorded at a constant current density of 1 mA/cm² is shown in Fig. 3. A marked polarization at the beginning of the reduction curve is a characteristic feature of the formation of new Li–Al alloy phase. This polarization is inferred that the initial formation of the new Li–Al alloy on the aluminum surface is difficult and needs additional power to accomplish this process. This phenomenon also could be found in the following cycles at various current

densities. The smooth reduction curve indicates that the process of lithium incorporation in aluminum substrate was stable. The potential drop in the middle of the chronopotentiometric curve is due to the polarization caused by the alternation of current direction, and the final sharp decrease of potential could be ascribed to the exhaustion of lithium in the Al electrode.

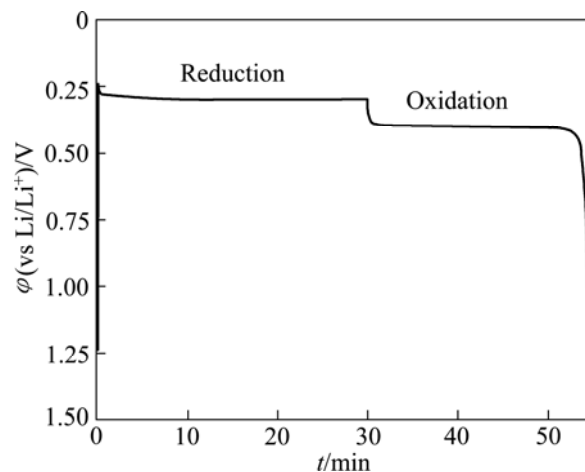


Fig. 3 Typical chronopotentiometric curve recorded during galvanostatic cycle experiment at 1 mA/cm² and 240 °C

Previous reports [26,27] have discussed that the efficiency of the lithium recoveries from aluminum is less than 100% due to the formation of Li–Al alloys. This phenomenon is the so-called “retention capacity” of Li–Al alloys. Normally, the “retention capacity” would result in very poor lithium recoveries in the first cycle. A similar result was obtained in our study, as presented in Fig. 4. The efficiency of the lithium recoveries can be determined from the ratio of time for oxidation to time for reduction by constant current measurements. The aluminum electrode was subjected to several cycles at

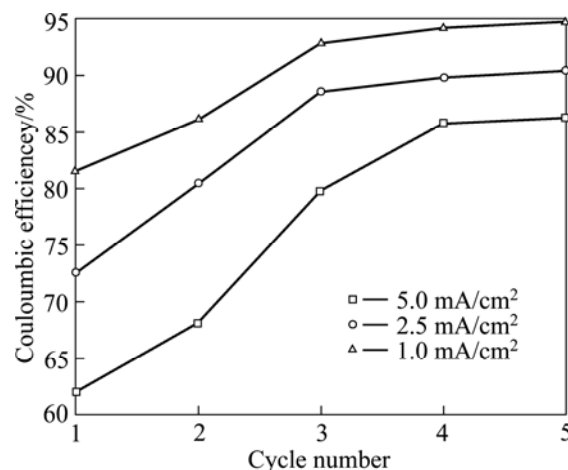


Fig. 4 Coulombic efficiency of anodic stripping of Li on Al electrode at 240 °C and various current densities

the current densities of 1.0, 2.5 and 5.0 mA/cm². At constant current densities, the coulombic efficiency could be calculated from the ratio of the time for stripping of lithium to the time of deposition of lithium. At the current density of 1 mA/cm², the coulombic efficiency is about 81% in the first cycle, and reaches an almost constant value in the third cycle. It is noteworthy that the coulombic efficiency decreases when the current density increases, and the coulombic efficiency tends to be the constant value after several cycles at the current densities of 2.5 and 5.0 mA/cm². It is noticeable that the processes of lithium incorporation in aluminum are also free from dendrites at the current densities of 1.0, 2.5 and 5.0 mA/cm² during charge–discharge cycles.

3.3 XRD and SEM micrographs

To prove the existence of Li–Al alloy after the charge–discharge cycles, an aluminum electrode was transferred from the cell for XRD and SEM measurements. Figure 5 shows XRD patterns of unused Al and electrochemically formed Li–Al specimens. Three peaks with a value of 2θ around 38.4°, 44.8° and 78.2° can be assigned to planes (111), (200) and (311) of Al, respectively. There are additional peaks at 40.3°, 43.2°, 50.4° and 74.1° which correspond to the Li–Al composition. SEM images of Al and electrochemically formed Li–Al alloy are shown in Fig. 6. The surface of the pure Al foil is smooth and cracks cannot be found, as presented in Fig. 6(a). The charge–discharge cycles in the LiTFSI/KTf molten salt electrolyte led to a significant change in the surface image from the original one. It is shown that the cracks are distributed over the surface of the electrochemically formed Li–Al alloy in Fig. 6(b). The cracks may be caused by the gradual increase of the electrode volume during the formation of Li–Al alloy.

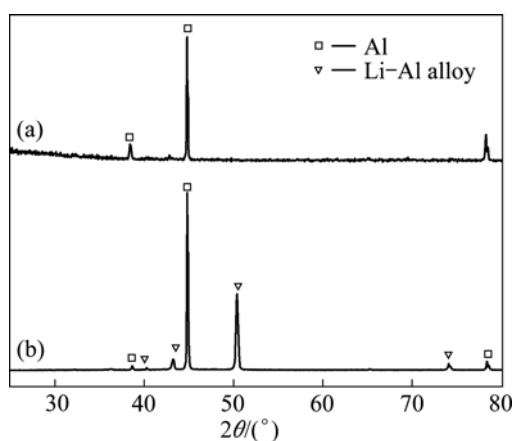


Fig. 5 XRD patterns of Al (a) and electrochemically formed Li–Al alloy (b) at 1 mA/cm² and 240 °C

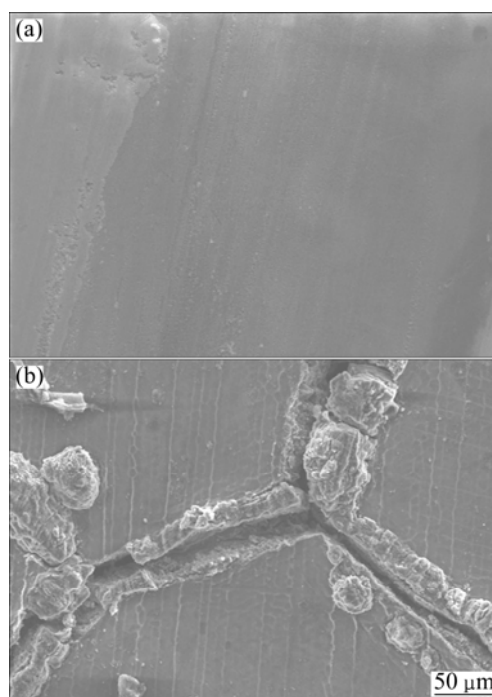


Fig. 6 SEM images of Al (a) and electrochemically formed Li–Al alloy (b) at 1 mA/cm² and 240 °C

3.4 Mechanism of lithium incorporation into Al electrode

More insight into the mechanism of Li incorporation into Al matrix can be attained from an analysis of chronoamperometry measurements which have been proved to be a convenient technique for the investigation of lithium reduction on the aluminum substrate. A typical chronoamperogram observed at a fresh Al electrode in the LiTFSI/KTf molten salt electrolyte is shown in Fig. 7. Two distinct regions (*A* and *B*) in the chronoamperogram could be observed. The initial part (*A*) of the reduction curve is characterized by a rapid decrease in the current to a minimum value. This

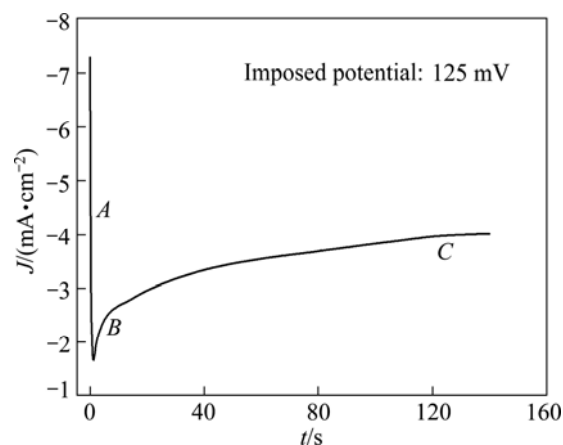


Fig. 7 Chronoamperogram on aluminum electrode in LiTFSI/KTf molten salt electrolyte at 240 °C

could be ascribed to the double-layer charging, and is more probably due to the insertion of lithium into aluminum matrix for the formation of α -phase Li–Al alloy [28,29].

The curves of current density (J) vs negative square root of time ($t^{-1/2}$) for the incorporation of Li into Al are presented in Fig. 8(a). The linearity of the curves indicates that this process is diffusion control. The diffusion coefficient of lithium penetration in aluminum for the formation of α -phase Li–Al alloy can be calculated from the Cottrell equation:

$$J(t) = nFS(c_t - c_0) \sqrt{\frac{D}{\pi t}} \quad (1)$$

where F denotes the Faraday constant; c_t is the saturated concentration of lithium in the α -phase Li–Al alloy; c_0 is the initial lithium concentration in aluminum; D is the diffusion coefficient. The charge transfer number n is equal to 1 and c_0 is assumed to be zero. Then Eq. (1) can be simplified to

$$J(t) = FSc_t \sqrt{\frac{D}{\pi t}} \quad (2)$$

Thus the diffusion coefficient D is $1.8 \times 10^{-10} \text{ cm}^2/\text{s}$

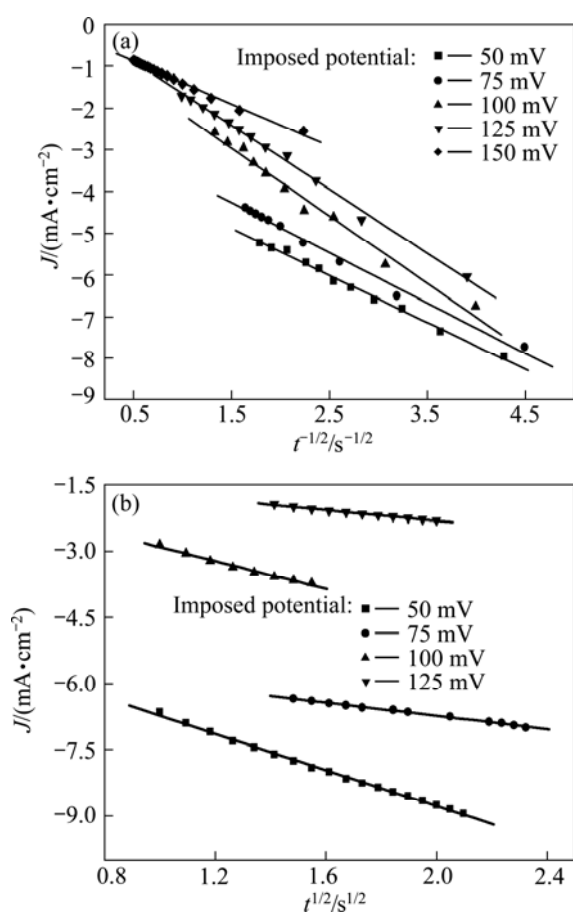


Fig. 8 Portions of cathodic chronoamperograms on aluminum electrode in LiTFSI/KTf molten salt electrolyte at 240 °C: (a) Initial current decay region; (b) Current increase region

which is calculated from the curve of the imposed potential of 125 mV at 240 °C. This experimental value of D is lower than the value ($D=4.0 \times 10^{-10} \text{ cm}^2/\text{s}$) obtained at 450 °C in the LiCl–KCl melt [30], but higher than that ($D=2.4 \times 10^{-11} \text{ cm}^2/\text{s}$) obtained at 20 °C in 1 mol/L LiClO₄/PC solution [28]. This is in good agreement with the trend that the diffusion coefficient D gradually increases with the increase of temperature. The following part (B) of the cathodic chronoamperogram shows a slower increase in current, which should correspond to the formation and growth of the nuclei on the surface. The curves of current density (J) vs the square root of time ($t^{1/2}$) are depicted in Fig. 8(b). It is shown that the curves are linear at the various potentials, which may provide the evidence for the instantaneous three-dimensional nucleation [31]. As we know, the instantaneous three-dimensional nucleation theory has been developed for the electrodeposition in which the substrate electrode itself does not change. Thus, the process of lithium incorporation into aluminum remains dubious and needs further investigations.

4 Conclusions

1) The initial steps of lithium incorporation into aluminum appear to involve a nucleation process. The incorporation of lithium into aluminum is uniform and smooth.

2) The coulombic efficiency is very low in the first cycle and arrives the constant values after several cycles at the current densities of 1.0, 2.5 and 5.0 mA/cm².

3) The incorporation of lithium into aluminum for the formation of α -phase Li–Al alloy is limited by its diffusion coefficient. The diffusion coefficient of lithium incorporation into aluminum was measured to be $1.8 \times 10^{-10} \text{ cm}^2/\text{s}$.

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LiTFSi/KTf 熔盐电解质中锂在铝电极上的电化学反应

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摘要: 采用循环伏安、计时电位和计时电流等电化学测试技术考察 LiTFSi/KTf 熔盐电解质中锂在铝电极上的电化学反应。结果表明: 在该熔盐中, 锂在铝电极上的电化学反应过程伴随着锂铝合金的成核过程, 锂在铝电极上的嵌入过程平缓、稳定。恒电流充放电循环实验发现, 首次循环的库仑效率很低, 这主要归结于 Li–Al 合金对锂元素的持留能力。通过 XRD 和 SEM 表征了充放电前后铝电极的物相组成和表面形貌。计时电流实验发现, 锂离子嵌入铝电极中形成 α -Li–Al 合金的过程受锂在铝基体内的扩散步骤控制, 且该扩散系数为 $1.8 \times 10^{-10} \text{ cm}^2/\text{s}$ 。

关键词: 熔盐; 铝电极; 循环伏安; 库仑效率; 成核过程

(Edited by YANG Hua)